

Propanoic acid

Other names:	Acide propionique
	Antischim B
	C2H5COOH
	CARBOXYETHANE
	ETHYLFORMIC ACID
	Ethancarboxylic acid
	Kyselina propionova
	LUPRISOL
	Luprosil
	Metacetonc acid
	Methylacetic acid
	MonoProp
	PROPIONIC ACID
	Propcorn
	Propionic acid grain preserver
	Propkorn
	Prozoin
	Pseudoacetic acid
	Sentry grain preserver
	Tenox P grain preservative
	UN 1848
	n-Propionic acid
Inchi:	InChI=1S/C3H6O2/c1-2-3(4)5/h2H2,1H3,(H,4,5)
InchiKey:	XBDQKXXYIPTUBI-UHFFFAOYSA-N
Formula:	C3H6O2
SMILES:	CCC(=O)O
Mol. weight [g/mol]:	74.08
CAS:	79-09-4

Physical Properties

Property code	Value	Unit	Source
af	0.5200		KDB
affp	797.20	kJ/mol	NIST Webbook
aigt	869.26	K	KDB
basg	766.20	kJ/mol	NIST Webbook
chl	-1528.00	kJ/mol	NIST Webbook

chl	-1527.30 ± 0.10	kJ/mol	NIST Webbook
dm	1.50	debye	KDB
fll	2.90	% in Air	KDB
flu	14.80	% in Air	KDB
fpc	329.82	K	KDB
fpo	327.59	K	KDB
gf	-369.60	kJ/mol	KDB
gyrad	3.0500		KDB
hf	-455.80 ± 2.00	kJ/mol	NIST Webbook
hf	-455.00 ± 3.20	kJ/mol	NIST Webbook
hf	-455.80 ± 2.00	kJ/mol	NIST Webbook
hf	-455.40	kJ/mol	KDB
hfl	-510.00 ± 2.50	kJ/mol	NIST Webbook
hfl	-510.80 ± 0.10	kJ/mol	NIST Webbook
hfus	9.21	kJ/mol	Joback Method
hvap	54.40	kJ/mol	NIST Webbook
hvap	55.00 ± 2.00	kJ/mol	NIST Webbook
hvap	30.60 ± 0.02	kJ/mol	NIST Webbook
hvap	54.90	kJ/mol	NIST Webbook
hvap	55.00	kJ/mol	NIST Webbook
hvap	55.00 ± 2.00	kJ/mol	NIST Webbook
ie	10.44 ± 0.06	eV	NIST Webbook
ie	10.40	eV	NIST Webbook
ie	10.51	eV	NIST Webbook
ie	10.41	eV	NIST Webbook
ie	10.41	eV	NIST Webbook
ie	10.53 ± 0.00	eV	NIST Webbook
ie	10.54	eV	NIST Webbook
ie	10.44 ± 0.03	eV	NIST Webbook
ie	10.24 ± 0.03	eV	NIST Webbook
ie	10.51	eV	NIST Webbook
ie	10.72	eV	NIST Webbook
log10ws	-0.18		Crippen Method
logp	0.481		Crippen Method
mcvol	60.570	ml/mol	McGowan Method
nfpaf	%!d(float64=2)		KDB
nfpah	%!d(float64=2)		KDB
pc	4668.00 ± 50.00	kPa	NIST Webbook
pc	4810.14 ± 90.00	kPa	NIST Webbook
pc	4060.00 ± 405.30	kPa	NIST Webbook
pc	4530.00	kPa	KDB
pc	5360.00 ± 506.63	kPa	NIST Webbook
pc	4530.00 ± 50.00	kPa	NIST Webbook
rhoc	314.83 ± 5.93	kg/m3	NIST Webbook

rhoc	334.09 ± 3.33	kg/m3	NIST Webbook
rinpol	683.00		NIST Webbook
rinpol	684.00		NIST Webbook
rinpol	721.00		NIST Webbook
rinpol	702.00		NIST Webbook
rinpol	693.00		NIST Webbook
rinpol	748.00		NIST Webbook
rinpol	743.00		NIST Webbook
rinpol	743.00		NIST Webbook
rinpol	717.00		NIST Webbook
rinpol	721.00		NIST Webbook
rinpol	690.00		NIST Webbook
rinpol	729.00		NIST Webbook
rinpol	681.00		NIST Webbook
rinpol	668.00		NIST Webbook
rinpol	679.00		NIST Webbook
rinpol	732.00		NIST Webbook
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rinpol	725.00		NIST Webbook
rinpol	739.00		NIST Webbook
rinpol	668.00		NIST Webbook
rinpol	740.00		NIST Webbook
rinpol	693.00		NIST Webbook
rinpol	745.00		NIST Webbook
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rinpol	702.00		NIST Webbook
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rinpol	717.00		NIST Webbook
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rinpol	700.00		NIST Webbook
rinpol	695.00		NIST Webbook
rinpol	710.00		NIST Webbook
rinpol	711.00		NIST Webbook

ripol	1498.00	NIST Webbook
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ripol	1535.00	NIST Webbook
ripol	1486.00	NIST Webbook
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ripol	1556.00	NIST Webbook
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ripol	1531.00	NIST Webbook
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ripol	1536.00		NIST Webbook
ripol	1543.00		NIST Webbook
ripol	1543.00		NIST Webbook
ripol	1534.00		NIST Webbook
ripol	1560.00		NIST Webbook
ripol	1564.00		NIST Webbook
ripol	1547.00		NIST Webbook
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ripol	1534.00		NIST Webbook
ripol	1541.00		NIST Webbook
ripol	1526.00		NIST Webbook
ripol	1523.00		NIST Webbook
ripol	1518.00		NIST Webbook
ripol	1554.00		NIST Webbook
ripol	1539.00		NIST Webbook
ripol	1525.00		NIST Webbook
ripol	1555.00		NIST Webbook
ripol	1531.00		NIST Webbook
ripol	1570.00		NIST Webbook
ripol	1538.00		NIST Webbook
ripol	1538.00		NIST Webbook
ripol	1540.00		NIST Webbook
ripol	1573.00		NIST Webbook
ripol	1553.00		NIST Webbook
ripol	1544.00		NIST Webbook
ripol	1540.00		NIST Webbook
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ripol	1534.00		NIST Webbook
ripol	1508.00		NIST Webbook
ripol	1498.00		NIST Webbook
ripol	1528.00		NIST Webbook
ripol	1561.00		NIST Webbook
sl	191.00	J/mol×K	NIST Webbook
tb	414.30	K	KDB
tb	414.45 ± 1.00	K	NIST Webbook
tb	412.55 ± 1.00	K	NIST Webbook
tb	413.85 ± 0.60	K	NIST Webbook
tb	414.05 ± 0.60	K	NIST Webbook

tb	413.45 ± 0.40	K	NIST Webbook
tb	414.95 ± 0.60	K	NIST Webbook
tb	414.00 ± 0.60	K	NIST Webbook
tb	413.15 ± 1.00	K	NIST Webbook
tb	415.55 ± 2.00	K	NIST Webbook
tb	414.35	K	Determination and correlation of liquid liquid equilibria for the (water + carboxylic acid + dimethyl maleate) ternary systems at T = 298.2K
tb	413.58	K	Multiphase equilibria for mixtures containing water, isopropanol, propionic acid, and isopropyl propionate
tb	414.25	K	Quaternary phase equilibrium of water-carboxylic acid mixture (formic-propionic acid or acetic-propionic acid)-solvent liquid systems at 298.15 K
tb	414.20	K	Ternary liquid-liquid phase equilibria of (water-carboxylic acid-1-undecanol) systems at 298.15 K
tb	414.01	K	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tb	414.10	K	(Liquid + liquid) equilibria of (water + propionic acid + dimethyl phthalate) at several temperatures
tb	414.10	K	(Liquid + liquid) equilibria of (water + propionic acid + diethyl phthalate) at several temperatures
tb	414.10	K	(Liquid + liquid) equilibria of (water + propionic acid + cyclohexanone) at several temperatures
tb	414.50	K	(Liquid + liquid) equilibria of (water + propionic acid + alcohol) ternary systems
tb	414.30	K	(Liquid + liquid) equilibria of (water + propionic acid + dipropyl ether or diisopropyl ether) at T = 298.2 K
tb	414.50	K	(Liquid + liquid) equilibria of (water + propionic acid + diethyl succinate or diethyl glutarate or diethyl adipate) ternary systems

tb	414.10	K	(Liquid + liquid) equilibria of (water + propionic acid + 2-ethyl-1-hexanol): Experimental data and correlation
tb	414.32	K	Isobaric vapour-liquid equilibrium for binary systems of ethyl iodide with ethanol, propionic acid and ethyl propionate at 101.3 kPa
tb	414.35	K	Solubility and critical surface in the system propionic acid-ethanol-ethyl propionate-water at 293.15, 303.15 and 313.15 K
tb	414.05	K	Measurements of Quaternary Liquid-Liquid Equilibrium for Water + Acetic Acid + Propionic Acid + Solvent (Butyronitrile, Benzyl Acetate, or Methyl Isobutyl Ketone) at 298.15 K
tb	414.01 ± 0.50	K	NIST Webbook
tb	414.20	K	NIST Webbook
tb	413.85 ± 0.60	K	NIST Webbook
tb	414.50 ± 0.15	K	NIST Webbook
tb	414.50 ± 0.15	K	NIST Webbook
tb	414.15 ± 0.50	K	NIST Webbook
tb	414.00 ± 0.20	K	NIST Webbook
tb	414.10 ± 0.30	K	NIST Webbook
tb	413.90 ± 0.30	K	NIST Webbook
tb	414.20 ± 1.50	K	NIST Webbook
tb	414.00 ± 2.00	K	NIST Webbook
tb	413.95	K	NIST Webbook
tb	414.05 ± 0.50	K	NIST Webbook
tb	414.20 ± 0.20	K	NIST Webbook
tb	413.70 ± 0.40	K	NIST Webbook
tb	413.85 ± 0.40	K	NIST Webbook
tb	414.05 ± 0.20	K	NIST Webbook
tb	413.86 ± 0.50	K	NIST Webbook
tb	412.65 ± 1.00	K	NIST Webbook
tb	414.67 ± 0.40	K	NIST Webbook
tb	414.45 ± 0.50	K	NIST Webbook
tb	412.90 ± 0.60	K	NIST Webbook
tb	414.25 ± 0.50	K	NIST Webbook
tb	414.25 ± 0.60	K	NIST Webbook
tb	414.15 ± 0.50	K	NIST Webbook
tb	413.60 ± 0.40	K	NIST Webbook

tb	414.15 ± 1.50	K	NIST Webbook
tb	413.95 ± 0.30	K	NIST Webbook
tb	414.45 ± 0.50	K	NIST Webbook
tb	410.65 ± 2.00	K	NIST Webbook
tb	413.85 ± 0.30	K	NIST Webbook
tb	414.15 ± 1.00	K	NIST Webbook
tb	414.50 ± 0.50	K	NIST Webbook
tb	414.45 ± 0.50	K	NIST Webbook
tb	412.65 ± 2.00	K	NIST Webbook
tb	413.86 ± 0.60	K	NIST Webbook
tb	414.60 ± 0.60	K	NIST Webbook
tb	413.85 ± 0.30	K	NIST Webbook
tb	414.65 ± 0.30	K	NIST Webbook
tb	404.15 ± 5.00	K	NIST Webbook
tb	414.15 ± 2.00	K	NIST Webbook
tb	414.40 ± 0.20	K	NIST Webbook
tb	413.95 ± 0.60	K	NIST Webbook
tb	414.50 ± 0.20	K	NIST Webbook
tb	413.25 ± 1.00	K	NIST Webbook
tb	413.10 ± 0.30	K	NIST Webbook
tb	413.85 ± 0.60	K	NIST Webbook
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tb	413.85 ± 0.50	K	NIST Webbook
tb	413.65 ± 1.00	K	NIST Webbook
tb	412.75 ± 1.00	K	NIST Webbook
tb	414.15 ± 1.00	K	NIST Webbook
tb	414.20 ± 0.30	K	NIST Webbook
tb	412.15 ± 2.00	K	NIST Webbook
tb	414.40 ± 0.30	K	NIST Webbook
tb	414.45 ± 0.30	K	NIST Webbook
tb	413.45 ± 0.40	K	NIST Webbook
tc	598.50 ± 1.00	K	NIST Webbook
tc	602.20 ± 2.00	K	NIST Webbook
tc	613.10 ± 6.00	K	NIST Webbook
tc	612.70 ± 6.00	K	NIST Webbook
tc	599.95 ± 1.00	K	NIST Webbook
tc	610.80 ± 6.00	K	NIST Webbook
tc	604.00	K	KDB
tc	604.00 ± 0.50	K	NIST Webbook
tc	611.49 ± 2.50	K	NIST Webbook
tf	250.89	K	Determination of the solid liquid phase diagram of the binary system propionic acid / water
tf	252.40	K	KDB

tf	252.54	K	Solid liquid equilibrium in the ternary system acetic acid propanoic acid formamide
tf	252.32	K	The phase envelopes of alternative solvents (ionic liquid, CO ₂) and building blocks of biomass origin (lactic acid, propionic acid)
tf	251.95	K	Differential scanning calorimetry determination of phase diagrams and water activities of aqueous carboxylic acid solutions
tt	252.65	K	KDB
tt	252.65 ± 0.06	K	NIST Webbook
vc	0.222	m ³ /kmol	KDB
zc	0.2002520		KDB
zra	0.25		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	134.95	J/mol×K	559.90	Joback Method
cpg	139.21	J/mol×K	589.06	Joback Method
cpg	130.50	J/mol×K	530.74	Joback Method
cpg	125.86	J/mol×K	501.57	Joback Method
cpg	121.03	J/mol×K	472.41	Joback Method
cpg	116.00	J/mol×K	443.25	Joback Method
cpg	110.78	J/mol×K	414.09	Joback Method
cpl	152.80	J/mol×K	298.15	NIST Webbook
cpl	159.40	J/mol×K	289.00	NIST Webbook
cpl	151.00	J/mol×K	298.15	NIST Webbook
cpl	158.60	J/mol×K	298.15	NIST Webbook
cpl	154.60	J/mol×K	333.15	NIST Webbook
dvisc	0.0007062	Pa×s	323.15	Densities and Viscosities of Binary Mixtures of Propanoic Acid with N,N-Dimethylaniline and N,N-Diethylaniline at T = (303.15, 313.15, and 323.15) K

dvisc	0.0008476	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of Propanoic Acid with N,N-Dimethylaniline and N,N-Diethylaniline at T = (303.15, 313.15, and 323.15) K
dvisc	0.0009496	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of Propanoic Acid with N,N-Dimethylaniline and N,N-Diethylaniline at T = (303.15, 313.15, and 323.15) K
hfust	10.66	kJ/mol	252.70	NIST Webbook
hfust	10.66	kJ/mol	252.70	NIST Webbook
hsubt	73.00 ± 1.00	kJ/mol	233.00	NIST Webbook
hsubt	74.00 ± 1.00	kJ/mol	231.50	NIST Webbook
hvapt	47.00	kJ/mol	381.00	NIST Webbook
hvapt	60.60	kJ/mol	462.50	NIST Webbook
hvapt	48.30	kJ/mol	382.50	NIST Webbook
hvapt	56.00	kJ/mol	303.00	NIST Webbook
hvapt	46.40	kJ/mol	373.00	NIST Webbook
pvap	38.30	kPa	385.60	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	95.10	kPa	411.97	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid

pvap	101.21	kPa	413.74	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid
pvap	23.38	kPa	373.10	Vapor-Liquid Equilibria on Four Binary Systems: 2-Phenylpropionaldehyde + Phenol, Propylene Glycol Monomethyl Ether + Nitroethane, Dimethyl Ether + Propylene, and N-Butyric Acid + Propionic Acid
pvap	101.30	kPa	413.58	Multiphase equilibria for mixtures containing water, isopropanol, propionic acid, and isopropyl propionate
pvap	30.80	kPa	379.65	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	34.50	kPa	382.45	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	96.29	kPa	413.15	Vapor-Liquid Equilibria on Four Binary Systems: 2-Phenylpropionaldehyde + Phenol, Propylene Glycol Monomethyl Ether + Nitroethane, Dimethyl Ether + Propylene, and N-Butyric Acid + Propionic Acid

pvap	43.50	kPa	389.10	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	51.40	kPa	391.90	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	61.80	kPa	393.75	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	72.90	kPa	399.05	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	71.20	kPa	403.95	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	82.50	kPa	407.75	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	93.50	kPa	411.65	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa

pvap	105.30	kPa	415.45	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	112.70	kPa	417.65	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	101.30	kPa	414.32	Isobaric vapour-liquid equilibrium for binary systems of ethyl iodide with ethanol, propionic acid and ethyl propionate at 101.3 kPa
pvap	14.56	kPa	361.52	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid
pvap	19.58	kPa	368.37	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid
pvap	29.65	kPa	378.95	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid

pvap	39.73	kPa	386.74	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid
pvap	49.79	kPa	392.93	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid
pvap	59.86	kPa	398.09	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid
pvap	69.92	kPa	402.65	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid
pvap	79.99	kPa	406.80	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid

pvap	90.07	kPa	410.33	Subatmospheric Vapor Pressure Curves for Propionic Acid, Butyric Acid, Isobutyric Acid, Valeric Acid, Isovaleric Acid, Hexanoic Acid, and Heptanoic Acid
rfi	1.38484		298.15	Refractive Index, Surface Tension, and Density of Aqueous Mixtures of Carboxylic Acids at 298.15 K
rfi	1.38090		293.15	Isothermal vapour-liquid equilibrium data for the binary systems 2-propanone + (2-butanol or propanoic acid)
rfi	1.38350		293.15	Volumetric Properties of Highly Nonideal Binary Mixtures Containing Ethanoic Acid and Propanoic Acid with Butan-2-ol, Methyl-2-propanol, and 2-Methyl-2-butanol at Different Temperatures
rfi	1.38580		298.15	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Propanal, Propanol, and Propanoic Acid
rfi	1.38100		293.15	Vapour liquid equilibrium of carboxylic acid systems: Propionic acid + valeric acid and isobutyric acid + valeric acid
rfi	1.38110		293.15	Liquid liquid equilibria of ternary systems (water + carboxylic acid + cumene) at 298.15K

rfi	1.38110	293.15	(Liquid + liquid) equilibria of (water + propionic acid + methyl isoamyl ketone or diisobutyl ketone or ethyl isoamyl keton) at T = 298.2 K
rfi	1.38080	293.15	Liquid phase equilibria of (water + propionic acid + oleyl alcohol) ternary system at several temperatures
rfi	1.38200	298.20	Ternary liquid liquid equilibria for mixtures of an ionic liquid + n-hexane + an organic compound involved in the kinetic resolution of rac-1-phenyl ethanol (rac-1-phenyl ethanol, vinyl propionate, rac-1-phenylethyl propionate or propionic acid) at 298.2K and atmospheric pressure
rfi	1.38120	293.15	Vapour-liquid equilibrium of propionic acid + caproic acid, isobutyric acid + caproic acid, valeric acid + caproic acid and caproic acid + enanthoic acid binary mixtures
rfi	1.38290	303.15	Liquid liquid equilibria measurements of ternary systems (acetonitrile + a carboxylic acid + dodecane) at 303.15 K
rfi	1.38290	303.15	Phase equilibria measurements of ternary mixtures (sulfolane + a carboxylic acid + pentane) at 303.15 K

rfi	1.38610		298.15	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Methanol, Ethanoic Acid, and Propanoic Acid
rfi	1.38080		293.15	(Liquid + liquid) equilibria of (water + propionic acid + dibasic esters) ternary systems
rfi	1.38110		293.00	Quaternary Liquid-Liquid Equilibrium of Water + Acetic Acid + Propionic Acid + Solvent (Amyl Alcohol, Cyclohexyl Acetate, or Toluene) Systems
rhoI	977.67	kg/m3	308.15	Density, speed of sound, and refractive index measurements for the binary systems (butanoic acid + propanoic acid, or 2-methyl-propanoic acid) at T = (293.15 to 313.15) K
rhoI	977.04	kg/m3	308.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure

rhoI	971.63	kg/m3	313.14	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	966.24	kg/m3	318.14	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	993.00	kg/m3	293.00	KDB
rhoI	988.04	kg/m3	298.20	(Liquid + liquid) equilibria of the (water + carboxylic acid + dibasic esters mixture (DBE-2)) ternary systems
rhoI	988.10	kg/m3	298.20	Phase equilibria of (water + propionic acid or butyric acid + 2-methoxy-2-methylpropane) ternary systems at 298.2 K and 323.2 K
rhoI	993.88	kg/m3	293.15	Density, speed of sound, and refractive index measurements for the binary systems (butanoic acid + propanoic acid, or 2-methyl-propanoic acid) at T = (293.15 to 313.15) K

rhoI	988.48	kg/m3	298.15	Density, speed of sound, and refractive index measurements for the binary systems (butanoic acid + propanoic acid, or 2-methyl-propanoic acid) at T = (293.15 to 313.15) K
rhoI	983.07	kg/m3	303.15	Density, speed of sound, and refractive index measurements for the binary systems (butanoic acid + propanoic acid, or 2-methyl-propanoic acid) at T = (293.15 to 313.15) K
rhoI	960.84	kg/m3	323.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	972.27	kg/m3	313.15	Density, speed of sound, and refractive index measurements for the binary systems (butanoic acid + propanoic acid, or 2-methyl-propanoic acid) at T = (293.15 to 313.15) K
rhoI	993.90	kg/m3	293.15	Effect of temperature on density, sound velocity, refractive index and their derived properties for the binary systems (heptanoic acid + propanoic or butanoic acids)

rhoI	988.50	kg/m3	298.15	Effect of temperature on density, sound velocity, refractive index and their derived properties for the binary systems (heptanoic acid + propanoic or butanoic acids)
rhoI	983.10	kg/m3	303.15	Effect of temperature on density, sound velocity, refractive index and their derived properties for the binary systems (heptanoic acid + propanoic or butanoic acids)
rhoI	977.70	kg/m3	308.15	Effect of temperature on density, sound velocity, refractive index and their derived properties for the binary systems (heptanoic acid + propanoic or butanoic acids)
rhoI	972.30	kg/m3	313.15	Effect of temperature on density, sound velocity, refractive index and their derived properties for the binary systems (heptanoic acid + propanoic or butanoic acids)
rhoI	987.90	kg/m3	298.15	Speed of sound as a function of temperature and pressure for propane derivatives
rhoI	998.04	kg/m3	298.15	Liquid Phase Equilibria of Aqueous Mixtures of Carboxylic Acids (C1-C4) with Ethylbenzene: Thermodynamic and Mathematical Modeling

rhoI	988.00	kg/m3	293.15	Correlation of Experimental Liquid Liquid Equilibrium Data for Ternary Systems Using NRTL and GMDH-Type Neural Network	
rhoI	993.80	kg/m3	293.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid	
rhoI	988.40	kg/m3	298.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid	
rhoI	983.00	kg/m3	303.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid	
rhoI	977.60	kg/m3	308.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid	
rhoI	972.20	kg/m3	313.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid	
rhoI	1004.11	kg/m3	283.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure	

rhoI	998.69	kg/m3	288.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	993.26	kg/m3	293.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	987.85	kg/m3	298.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	982.44	kg/m3	303.14	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	993.72	kg/m3	298.15	Phase Equilibria for Reactive Distillation of Propyl Propanoate. Pure Component Property Data, Vapor-Liquid Equilibria, and Liquid-Liquid Equilibria

srf	0.03	N/m	293.15	Apparent Molar Volume and Surface Tension of Dilute Aqueous Solutions of Carboxylic Acids	
srf	0.03	N/m	298.15	Apparent Molar Volume and Surface Tension of Dilute Aqueous Solutions of Carboxylic Acids	
srf	0.03	N/m	303.15	Apparent Molar Volume and Surface Tension of Dilute Aqueous Solutions of Carboxylic Acids	
srf	0.03	N/m	308.15	Apparent Molar Volume and Surface Tension of Dilute Aqueous Solutions of Carboxylic Acids	

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	368.83	K	20.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa

tdp	378.94	K	30.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tdp	386.59	K	40.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tdp	392.77	K	50.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tdp	397.99	K	60.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tdp	402.56	K	70.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa

tbp	406.60	K	80.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	410.26	K	90.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	416.68	K	110.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	419.53	K	120.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	422.18	K	130.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa

tbp	424.67	K	140.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	427.01	K	150.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	429.23	K	160.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	431.36	K	170.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	433.37	K	180.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa

tbp	435.31	K	190.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa
tbp	437.16	K	200.00	Vapor-liquid equilibrium of isoamyl alcohol + isoamyl propionate and propionic acid + isoamyl propionate systems at 50.00, 101.33 and 150.00 kPa

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.56739e+01
Coeff. B	-3.98399e+03
Coeff. C	-5.36380e+01
Temperature range (K), min.	312.57
Temperature range (K), max.	600.81

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$
Coeff. A	7.77767e+01
Coeff. B	-8.37511e+03
Coeff. C	-8.90331e+00
Coeff. D	4.15966e-06
Temperature range (K), min.	252.45
Temperature range (K), max.	604.00

Sources

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<https://www.doi.org/10.1016/j.jct.2017.03.018>

<https://www.doi.org/10.1016/j.fluid.2015.03.039>

<https://www.doi.org/10.1016/j.fluid.2012.05.002>

<https://www.doi.org/10.1021/acs.jced.5b00632>

<https://www.doi.org/10.1021/je0604277>

<https://www.doi.org/10.1016/j.jct.2014.06.004>

<http://pubs.acs.org/doi/abs/10.1021/ci990307l>

<https://www.doi.org/10.1016/j.tca.2008.10.013>

<https://www.doi.org/10.1021/je3001969>

<https://www.doi.org/10.1021/je100912t>

<http://link.springer.com/article/10.1007/BF02311772>

<https://www.doi.org/10.1016/j.tca.2012.04.020>

<https://www.doi.org/10.1021/je101302p>

<https://www.doi.org/10.1021/acs.jced.5b00214>

<https://www.doi.org/10.1016/j.fluid.2014.03.002>

<https://www.doi.org/10.1016/j.jct.2006.05.001>

<https://www.doi.org/10.1021/je0496488>

<https://www.chemeo.com/doc/models/crippen> log10ws

<https://www.doi.org/10.1021/acs.jced.8b00043>

<https://www.doi.org/10.1021/je049848j>

<https://www.doi.org/10.1021/je050527x>

<https://www.doi.org/10.1021/acs.jced.6b00985>

<https://www.doi.org/10.1016/j.fluid.2011.01.020>

<https://www.doi.org/10.1016/j.fluid.2014.04.026>

<https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure>

<https://www.doi.org/10.1016/j.jct.2005.02.005>

<https://www.doi.org/10.1016/j.fluid.2014.12.013>

<https://www.doi.org/10.1016/j.fluid.2006.10.004>

<https://www.doi.org/10.1021/je200862b>

<https://www.doi.org/10.1016/j.jct.2007.02.012>

<https://www.doi.org/10.1021/je050327l>

<https://www.doi.org/10.1016/j.fluid.2015.06.029>

<https://www.doi.org/10.1016/j.jct.2019.07.002>

<https://www.doi.org/10.1016/j.fluid.2015.06.003>

<https://www.doi.org/10.1016/j.fluid.2008.07.004>

<https://www.doi.org/10.1021/je034180e>

<https://www.doi.org/10.1016/j.jct.2018.12.026>

<https://www.doi.org/10.1016/j.fluid.2011.09.014>

<https://www.doi.org/10.1016/j.fluid.2016.05.033>

[illegible]

<https://www.doi.org/10.1021/je060084c>
<https://www.doi.org/10.1021/je201102x>
<https://www.doi.org/10.1016/j.jct.2019.06.033>
<https://www.doi.org/10.1016/j.fluid.2015.04.014>
<https://www.doi.org/10.1021/je800796h>
<https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=931>
<https://www.doi.org/10.1016/j.jct.2007.03.004>
<https://www.doi.org/10.1016/j.jct.2015.12.019>
<https://www.doi.org/10.1016/j.fluid.2018.12.035>
<https://www.doi.org/10.1021/je030102f>
<https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=931>
<https://www.doi.org/10.1016/j.jct.2010.05.014>
<https://www.doi.org/10.1016/j.fluid.2016.10.024>
<https://www.doi.org/10.1016/j.fluid.2012.06.020>
<https://www.doi.org/10.1016/j.fluid.2005.08.006>
<https://www.doi.org/10.1016/j.fluid.2006.07.011>
<https://www.doi.org/10.1021/acs.jced.8b01204>
<https://www.doi.org/10.1016/j.fluid.2006.10.005>
<https://www.doi.org/10.1016/j.fluid.2017.12.023>
<https://www.doi.org/10.1021/je034250h>
<https://www.doi.org/10.1016/j.jct.2015.05.004>
<http://webbook.nist.gov/cgi/cbook.cgi?ID=C79094&Units=SI>
<https://www.doi.org/10.1016/j.fluid.2008.04.014>
<https://www.doi.org/10.1016/j.tca.2018.03.002>
<https://www.doi.org/10.1016/j.jct.2005.03.017>
<https://www.doi.org/10.1016/j.fluid.2004.10.029>
<https://www.doi.org/10.1016/j.jct.2009.08.014>
<https://www.doi.org/10.1016/j.fluid.2007.10.011>
<https://www.doi.org/10.1016/j.fluid.2010.01.018>
<https://www.doi.org/10.1016/j.fluid.2013.07.024>
<https://www.doi.org/10.1016/j.jct.2008.01.001>
<https://www.doi.org/10.1021/acs.jced.7b00431>
<https://www.doi.org/10.1021/acs.jced.6b00112>
<https://www.doi.org/10.1016/j.jct.2016.12.014>
<https://www.doi.org/10.1016/j.jct.2004.12.003>
<https://www.doi.org/10.1016/j.jct.2018.12.023>
<https://www.doi.org/10.1016/j.jct.2009.02.004>
<https://www.doi.org/10.1016/j.jct.2013.05.028>
<https://www.doi.org/10.1016/j.jct.2012.07.019>
<https://www.doi.org/10.1016/j.fluid.2011.03.003>
<https://www.doi.org/10.1016/j.jct.2003.11.011>
<https://www.doi.org/10.1016/j.fluid.2015.01.004>
<https://www.doi.org/10.1016/j.jct.2016.03.019>

Understanding ion-ion and ion-solvent interactions in aqueous solutions of tripropylamine and tripropylamine-based ionic liquids of water through protonic acid-base catalysis of propionic acid decomposition for gasification processes at 200-250 °C: temperature and pressure for propane derivatives equilibrium in systems (water + organic solvent + salt) at low water content and surface of Tension of Dilute Aqueous Solutions of Salts: Determination and correlation of cyromazine in sixteen pure solvents and binary mixtures: Data KDB Young Properties Data
 Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Methanol, Ethanoic Acid, and Propionic Acid with 1,1,1-Trichloro-2,2,2-trifluoroethane (HFC-133a) and 2,2,3,3-Tetrafluoropropane (HFO-1234ze) at 293.2 to 323.2 K
 Solid-liquid equilibrium in the ternary system acetic acid propanoic acid formic acid envelopes of alternative solvents (ionic liquid, CO₂) and Solid-Liquid Phase Diagrams of Binary (acetic acid propanoic acid) and ternary (acetic acid propanoic acid) mixtures at atmospheric pressure and different temperatures:

<https://www.doi.org/10.1016/j.fluid.2017.05.005>
<https://www.doi.org/10.1016/j.jct.2006.05.005>
<https://www.doi.org/10.1016/j.jct.2016.12.016>
<https://www.doi.org/10.1016/j.fluid.2004.07.017>
<https://www.doi.org/10.1021/je1002829>
<https://www.doi.org/10.1016/j.fluid.2018.07.024>
<https://www.thermo.com/research/kdb/hcprop/showprop.php?cmpid=931>
<https://www.doi.org/10.1021/je1000473>
<https://www.doi.org/10.1021/je500291x>
https://en.wikipedia.org/wiki/Joback_method
<https://www.doi.org/10.1016/j.fluid.2007.07.065>
<https://www.doi.org/10.1016/j.fluid.2010.05.013>
<https://www.doi.org/10.1016/j.fluid.2012.07.014>

Legend

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fl:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hsubt:	Enthalpy of sublimation at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient

mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhof:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sl:	Liquid phase molar entropy at standard conditions
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter

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