

# 2,5,8,11-Tetraoxadodecane

<b>Other names:</b>	(CH <sub>3</sub> O(CH <sub>2</sub> ) <sub>2</sub> OCH <sub>2</sub> ) <sub>2</sub> 1,2-Bis(2-methoxyethoxy)ethane 1,2-Bis(methoxyethoxy)ethane Ansul Ether 161 Dimethyl ether of triethylene glycol Ethane, 1,2-bis(2-methoxyethoxy)- Glyme 4 Glyme-3 NSC 66400 Triethylene glycol dimethyl ether Triglyme methyltriglyme triethylene glycol, dimethyl ether triglyme (triethylene glycol dimethyl ether)
<b>Inchi:</b>	InChI=1S/C8H18O4/c1-9-3-5-11-7-8-12-6-4-10-2/h3-8H2,1-2H3
<b>InchiKey:</b>	YFNKIDBQEZZDLK-UHFFFAOYSA-N
<b>Formula:</b>	C <sub>8</sub> H <sub>18</sub> O <sub>4</sub>
<b>SMILES:</b>	COCCOCCOCCOC
<b>Mol. weight [g/mol]:</b>	178.23
<b>CAS:</b>	112-49-2

## Physical Properties

Property code	Value	Unit	Source
affp	946.60	kJ/mol	NIST Webbook
basg	892.40	kJ/mol	NIST Webbook
gf	-403.52	kJ/mol	Joback Method
hf	-737.33	kJ/mol	Joback Method
hfus	21.23	kJ/mol	Joback Method
hvap	63.70 ± 3.30	kJ/mol	NIST Webbook
ie	9.80	eV	NIST Webbook
log10ws	0.48		Crippen Method
logp	0.312		Crippen Method
mcvol	147.060	ml/mol	McGowan Method
pc	2370.28	kPa	Joback Method
rinpol	1232.00		NIST Webbook
rinpol	1232.30		NIST Webbook
rinpol	208.42		NIST Webbook

rinpol	205.88		NIST Webbook
rinpol	1232.00		NIST Webbook
rinpol	205.88		NIST Webbook
rinpol	1232.30		NIST Webbook
sl	492.90	J/molxK	NIST Webbook
tb	489.15	K	NIST Webbook
tb	489.20	K	NIST Webbook
tb	489.00 ± 2.00	K	NIST Webbook
tb	489.00	K	NIST Webbook
tc	636.37	K	Joback Method
tf	228.00	K	NIST Webbook
tf	228.15	K	NIST Webbook
tt	229.30 ± 0.20	K	NIST Webbook
vc	0.555	m <sup>3</sup> /kmol	Joback Method

## Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	367.85	J/molxK	554.25	Joback Method
cpg	379.27	J/molxK	581.62	Joback Method
cpg	356.14	J/molxK	526.87	Joback Method
cpg	344.16	J/molxK	499.50	Joback Method
cpg	331.93	J/molxK	472.12	Joback Method
cpg	401.19	J/molxK	636.37	Joback Method
cpg	390.39	J/molxK	609.00	Joback Method
cpl	375.00	J/molxK	338.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
cpl	379.00	J/molxK	343.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K

cpl	373.00	J/mol×K	333.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
cpl	382.00	J/mol×K	353.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
cpl	367.78	J/mol×K	298.15	NIST Webbook
cpl	368.20	J/mol×K	298.15	NIST Webbook
cpl	359.00	J/mol×K	303.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
cpl	370.00	J/mol×K	323.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
cpl	368.00	J/mol×K	318.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K

cpl	366.00	J/molxK	313.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
cpl	364.00	J/molxK	308.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
cpl	381.00	J/molxK	348.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
cpl	371.00	J/molxK	328.15	Molar Heat Capacity of Aqueous Sulfolane, 4-Formylmorpholine, 1-Methyl-2-pyrrolidinone, and Triethylene Glycol Dimethyl Ether Solutions from (303.15 to 353.15) K
dvisc	0.0027500	Paxs	283.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0012500	Paxs	323.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0017800	Paxs	303.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0009360	Paxs	343.15	Density, viscosity and solubility of carbon dioxide in glymes

dvisc	0.0008210	Paxs	353.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0007260	Paxs	363.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0017700	Paxs	303.15	Densities, Viscosities and Derived Functions of Binary Mixtures: (Triethylene Glycol Dimethyl Ether + Water) and (N-acetylmorpholine+ Water) from 298.15 to 343.15 K
dvisc	0.0014800	Paxs	313.15	Densities, Viscosities and Derived Functions of Binary Mixtures: (Triethylene Glycol Dimethyl Ether + Water) and (N-acetylmorpholine+ Water) from 298.15 to 343.15 K
dvisc	0.0012600	Paxs	323.15	Densities, Viscosities and Derived Functions of Binary Mixtures: (Triethylene Glycol Dimethyl Ether + Water) and (N-acetylmorpholine+ Water) from 298.15 to 343.15 K
dvisc	0.0010800	Paxs	333.15	Densities, Viscosities and Derived Functions of Binary Mixtures: (Triethylene Glycol Dimethyl Ether + Water) and (N-acetylmorpholine+ Water) from 298.15 to 343.15 K

dvisc	0.0009450	Paxs	343.15	Densities, Viscosities and Derived Functions of Binary Mixtures: (Triethylene Glycol Dimethyl Ether + Water) and (N-acetylmorpholine+ Water) from 298.15 to 343.15 K
dvisc	0.0019600	Paxs	298.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0021900	Paxs	293.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0035600	Paxs	273.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0024500	Paxs	288.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0031000	Paxs	278.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0014800	Paxs	313.15	Density, viscosity and solubility of carbon dioxide in glymes
dvisc	0.0010800	Paxs	333.15	Density, viscosity and solubility of carbon dioxide in glymes
hfust	23.71	kJ/mol	229.30	NIST Webbook
hfust	23.71	kJ/mol	229.30	NIST Webbook
hfust	23.71	kJ/mol	229.30	NIST Webbook
rfi	1.41250		318.15	Liquid Densities and Refractive Indices of Binary Mixtures for the Dimethyl Ether of a Glycol + Ethanol from T=288.15 K to 318.15 K

rfi	1.42090		298.15	Liquid Densities and Refractive Indices of Binary Mixtures for the Dimethyl Ether of a Glycol + Ethanol from T=288.15 K to 318.15 K
rfi	1.41670		308.15	Liquid Densities and Refractive Indices of Binary Mixtures for the Dimethyl Ether of a Glycol + Ethanol from T=288.15 K to 318.15 K
rfi	1.42500		288.15	Liquid Densities and Refractive Indices of Binary Mixtures for the Dimethyl Ether of a Glycol + Ethanol from T=288.15 K to 318.15 K
rhoI	976.70	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhoI	971.90	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhoI	967.20	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhoI	962.40	kg/m3	318.15	Thermophysical properties of glycols and glymes
rhoI	957.70	kg/m3	323.15	Thermophysical properties of glycols and glymes
rhoI	952.90	kg/m3	328.15	Thermophysical properties of glycols and glymes
rhoI	948.10	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhoI	943.30	kg/m3	338.15	Thermophysical properties of glycols and glymes

rhoI	938.60	kg/m3	343.15	Thermophysical properties of glycols and glymes
rhoI	933.80	kg/m3	348.15	Thermophysical properties of glycols and glymes
rhoI	929.00	kg/m3	353.15	Thermophysical properties of glycols and glymes
rhoI	924.20	kg/m3	358.15	Thermophysical properties of glycols and glymes
rhoI	919.40	kg/m3	363.15	Thermophysical properties of glycols and glymes
rhoI	914.50	kg/m3	368.15	Thermophysical properties of glycols and glymes
rhoI	909.70	kg/m3	373.15	Thermophysical properties of glycols and glymes
rhoI	994.10	kg/m3	283.15	Thermophysical properties of glycols and glymes
rhoI	989.40	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhoI	984.60	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhoI	979.90	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhoI	986.00	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhoI	970.40	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhoI	965.60	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhoI	956.10	kg/m3	323.15	Thermophysical properties of glycols and glymes

rhoI	946.50	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhoI	936.90	kg/m3	343.15	Thermophysical properties of glycols and glymes
rhoI	980.62	kg/m3	298.15	Thermodynamics of Mixtures Containing Ethers. Part III. Liquid-Liquid Equilibria for 2,5,8,11-Tetraoxadodecane or 2,5,8,11,14-Pentaoxapentadecane + Selected N-Alkanes
rhoI	980.42	kg/m3	298.15	Liquid-Liquid Equilibrium of Ternary Mixtures Formed by Some Oligooxaethylenes with Ethanol and Hexadecane
rhoI	981.50	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhoI	975.10	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhoI	990.80	kg/m3	288.15	Thermophysical properties of glycols and glymes
sfust	103.40	J/molxK	229.30	NIST Webbook
srf	0.03	N/m	318.15	Volumetric and Surface Properties of Aqueous Mixtures of Polyethers at T = (298.15, 308.15, and 318.15) K
srf	0.03	N/m	308.15	Volumetric and Surface Properties of Aqueous Mixtures of Polyethers at T = (298.15, 308.15, and 318.15) K

srf	0.03	N/m	298.15	Volumetric and Surface Properties of Aqueous Mixtures of Polyethers at T = (298.15, 308.15, and 318.15) K
tcondl	0.13	W/m×K	362.39	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K
tcondl	0.14	W/m×K	302.75	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K
tcondl	0.12	W/m×K	392.16	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K
tcondl	0.14	W/m×K	332.54	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K

## Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbrp	376.70	K	1.30	NIST Webbook
tbrp	376.60	K	1.30	NIST Webbook

## Correlations

Information

Value

Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.57644e+01
Coeff. B	-4.62697e+03
Coeff. C	-7.40300e+01
Temperature range (K), min.	372.99
Temperature range (K), max.	516.68

## Datasets

### Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
293.15	100.00	1361.9
293.15	10000.00	1403.1
293.15	20000.00	1442.5
293.15	30000.00	1479.3
293.15	40000.00	1514.7
293.15	50000.00	1547.8
293.15	60000.00	1579.5
293.15	70000.00	1610.0
293.15	80000.00	1639.3
293.15	90000.00	1667.4
293.15	100000.00	1694.6
303.15	100.00	1323.2
303.15	10000.00	1366.5
303.15	20000.00	1407.2
303.15	30000.00	1445.2
303.15	40000.00	1481.6
303.15	50000.00	1515.7
303.15	60000.00	1548.2
303.15	70000.00	1579.4
303.15	80000.00	1609.3
303.15	90000.00	1638.2
303.15	100000.00	1665.9
313.15	100.00	1285.1
313.15	10000.00	1330.0
313.15	20000.00	1372.2
313.15	30000.00	1411.8

313.15	40000.00	1448.8
313.15	50000.00	1484.1
313.15	60000.00	1517.5
313.15	70000.00	1549.7
313.15	80000.00	1580.3
313.15	90000.00	1609.9
313.15	100000.00	1638.1
323.15	100.00	1247.7
323.15	10000.00	1294.6
323.15	20000.00	1338.5
323.15	30000.00	1379.1
323.15	40000.00	1417.3
323.15	50000.00	1453.6
323.15	60000.00	1487.9
323.15	70000.00	1520.7
323.15	80000.00	1552.0
323.15	90000.00	1581.9
323.15	100000.00	1610.8
333.15	100.00	1210.9
333.15	10000.00	1259.5
333.15	20000.00	1304.8
333.15	30000.00	1346.9
333.15	40000.00	1386.3
333.15	50000.00	1423.4
333.15	60000.00	1458.8
333.15	70000.00	1492.1
333.15	80000.00	1524.3
333.15	90000.00	1554.8
333.15	100000.00	1584.3
343.15	100.00	1174.6
343.15	10000.00	1225.1
343.15	20000.00	1272.0
343.15	30000.00	1315.6
343.15	40000.00	1356.2
343.15	50000.00	1394.1
343.15	60000.00	1430.3
343.15	70000.00	1464.6
343.15	80000.00	1497.2
343.15	90000.00	1528.4
343.15	100000.00	1558.5
353.15	100.00	1138.7
353.15	10000.00	1191.5
353.15	20000.00	1240.0
353.15	30000.00	1284.6

353.15	40000.00	1326.2
353.15	50000.00	1365.6
353.15	60000.00	1402.4
353.15	70000.00	1437.6
353.15	80000.00	1470.9
353.15	90000.00	1502.6
353.15	100000.00	1533.4

Reference

<https://www.doi.org/10.1021/je034036t>

## Viscosity, Pa\*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
293.15	100.00	0.0021350
293.15	20000.00	0.0025360
293.15	40000.00	0.0029700
293.15	60000.00	0.0034340
293.15	80000.00	0.0039260
293.15	100000.00	0.0044380
313.15	100.00	0.0014890
313.15	20000.00	0.0017550
313.15	40000.00	0.0020440
313.15	60000.00	0.0023550
313.15	80000.00	0.0026870
313.15	100000.00	0.0030400
333.15	100.00	0.0011200
333.15	20000.00	0.0013080
333.15	40000.00	0.0015010
333.15	60000.00	0.0016950
333.15	80000.00	0.0018890
333.15	100000.00	0.0020820
353.15	100.00	0.0008470
353.15	20000.00	0.0009880
353.15	40000.00	0.0011380
353.15	60000.00	0.0012960
353.15	80000.00	0.0014630
353.15	100000.00	0.0016390

Reference

<https://www.doi.org/10.1016/j.fluid.2006.06.015>

# Sources

Thermophysical properties of glycols and glymes: <https://www.doi.org/10.1021/acs.jced.5b00662>

Thermodynamics of Mixtures Containing Ethers. Part III. Isothermal Vapor-Liquid Equilibrium of the Absorption Working Pairs (HFC-32 + R123, HFC-32 + R1234yf, HFC-32 + R1234ze, HFC-32 + R124, HFC-32 + R1243ze, HFC-32 + R1243zf, HFC-32 + R1243ze + R1243zf, HFC-32 + R1243ze + R1243zf + R1243ze + R1243zf) at Temperatures from 293.15 to 343.15 K: The Yaws Handbook of Vapor Pressure: <http://webbook.nist.gov/cgi/cbook.cgi?ID=C112492&Units=SI>

NIST Webbook: <https://www.doi.org/10.1021/acs.jced.5b00782>

Measurement and Correlation of Isothermal Vapor Liquid Equilibrium of Fluoroalkane-Carbon Dioxide and Fluoroalkane-Alkyl Ethers at Different Temperatures: <https://www.doi.org/10.1021/je900641w>

Phase Equilibria of Fluoroethane + Diethyl Ether, Fluoroethane + Diethyl Ether + Tetrafluoroethane + Triethylene Glycol Dimethyl Ether, and Fluoroethane + Diethyl Ether + Tetrafluoroethane + Triethylene Glycol Dimethyl Ether within the Temperature Range of 293.15 to 343.15 K: <https://www.doi.org/10.1021/je100757w>

And Equilibrium Mixtures of Propanes at T = 298.15, 308.15, 318.15, and 328.15 K: <https://www.doi.org/10.1021/je800503d>

Equilibrium with Different Adsorbents: Mixtures Formed by Some Organic Pairs of Methane and Ethane in Promising Physical Solvents for Natural Gas Storage: <https://www.doi.org/10.1021/je050172h>

Sulfolane, 4-Formylmorpholine, Densities, Viscosities, and Derived Functions of Binary Dimethyl Ether Solutions with Carbon Dioxide, Ethanol, Water, and (N-acetylmorpholine + Water) from 298.15 to 343.15 K: <https://www.doi.org/10.1021/je020199q>

Triethylene Glycol Dimethyl Ether, Refractive Indices and Refractive Indices of Binary Mixtures to the Dimethyl Ether Measurements in Some Working Pairs for Gas Absorption Heat Transfer: <https://www.doi.org/10.1021/je9009915>

Phase Equilibria of Methane + Ethane + Carbon Dioxide in Glyme Diethylene Glycol Dimethyl Ether Equilibrium of the Absorption Working Pairs (R1234yf + R1234ze, R1234yf + R1234ze + R1234yf + R1234ze) at Temperatures from 293.15 to 343.15 K: <https://www.doi.org/10.1016/j.fluid.2010.08.014>

Phase Equilibria of Methane + Ethane + Carbon Dioxide in Glyme Diethylene Glycol Dimethyl Ether Equilibrium of the Absorption Working Pairs (R1234yf + R1234ze, R1234yf + R1234ze + R1234yf + R1234ze) at Temperatures from 293.15 to 343.15 K: <https://www.doi.org/10.1021/acs.jced.7b00821>

Phase Equilibria of Methane + Ethane + Carbon Dioxide in Glyme Diethylene Glycol Dimethyl Ether Equilibrium of the Absorption Working Pairs (R1234yf + R1234ze, R1234yf + R1234ze + R1234yf + R1234ze) at Temperatures from 293.15 to 343.15 K: <https://www.doi.org/10.1016/j.fluid.2006.06.015>

Phase Equilibria of Methane + Ethane + Carbon Dioxide in Glyme Diethylene Glycol Dimethyl Ether Equilibrium of the Absorption Working Pairs (R1234yf + R1234ze, R1234yf + R1234ze + R1234yf + R1234ze) at Temperatures from 293.15 to 343.15 K: <https://www.doi.org/10.1016/j.jct.2006.03.004>

Phase Equilibria of Methane + Ethane + Carbon Dioxide in Glyme Diethylene Glycol Dimethyl Ether Equilibrium of the Absorption Working Pairs (R1234yf + R1234ze, R1234yf + R1234ze + R1234yf + R1234ze) at Temperatures from 293.15 to 343.15 K: <https://www.doi.org/10.1021/je034036t>

Phase Equilibria of Methane + Ethane + Carbon Dioxide in Glyme Diethylene Glycol Dimethyl Ether Equilibrium of the Absorption Working Pairs (R1234yf + R1234ze, R1234yf + R1234ze + R1234yf + R1234ze) at Temperatures from 293.15 to 343.15 K: <http://link.springer.com/article/10.1007/BF02311772>

Phase Equilibria of Methane + Ethane + Carbon Dioxide in Glyme Diethylene Glycol Dimethyl Ether Equilibrium of the Absorption Working Pairs (R1234yf + R1234ze, R1234yf + R1234ze + R1234yf + R1234ze) at Temperatures from 293.15 to 343.15 K: [https://en.wikipedia.org/wiki/Joback\\_method](https://en.wikipedia.org/wiki/Joback_method)

Joback Method: [https://en.wikipedia.org/wiki/Joback\\_method](https://en.wikipedia.org/wiki/Joback_method)

## Legend

affp:	Proton affinity
basg:	Gas basicity
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dvisc:	Dynamic viscosity
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions

<b>hfust:</b>	Enthalpy of fusion at a given temperature
<b>hvac:</b>	Enthalpy of vaporization at standard conditions
<b>ie:</b>	Ionization energy
<b>log10ws:</b>	Log10 of Water solubility in mol/l
<b>logp:</b>	Octanol/Water partition coefficient
<b>mcvol:</b>	McGowan's characteristic volume
<b>pc:</b>	Critical Pressure
<b>pvap:</b>	Vapor pressure
<b>rfi:</b>	Refractive Index
<b>rho:</b>	Liquid Density
<b>rinpol:</b>	Non-polar retention indices
<b>sfust:</b>	Entropy of fusion at a given temperature
<b>sl:</b>	Liquid phase molar entropy at standard conditions
<b>speedsl:</b>	Speed of sound in fluid
<b>srf:</b>	Surface Tension
<b>tb:</b>	Normal Boiling Point Temperature
<b>tbrp:</b>	Boiling point at reduced pressure
<b>tc:</b>	Critical Temperature
<b>tcondl:</b>	Liquid thermal conductivity
<b>tf:</b>	Normal melting (fusion) point
<b>tt:</b>	Triple Point Temperature
<b>vc:</b>	Critical Volume

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