

Benzene

Other names:	1,3,5-Cyclohexatriene Benzeen Benzen Benzin Benzine Benzol Benzole Benzolene Benzolo Bicarburet of hydrogen Carbon oil Coal naphtha Cyclohexatriene Fenzen Mineral naphtha Motor benzol NCI-C55276 NSC 67315 Phene Phenyl hydride Pyrobenzol Pyrobenzole Rcra waste number U019 UN 1114 [6]Annulene
Inchi:	InChI=1S/C6H6/c1-2-4-6-5-3-1/h1-6H
InchiKey:	UHOVQNZJYSORNB-UHFFFAOYSA-N
Formula:	C6H6
SMILES:	c1ccccc1
Mol. weight [g/mol]:	78.11
CAS:	71-43-2

Physical Properties

Property code	Value	Unit	Source
af	0.2120		KDB
affp	750.40	kJ/mol	NIST Webbook

affp	746.40	kJ/mol	NIST Webbook
aigt	864.82	K	KDB
basg	721.70	kJ/mol	NIST Webbook
basg	725.40	kJ/mol	NIST Webbook
dm	0.00	debye	KDB
dvisc	0.0006080	Paxs	Densities and Viscosities of Binary Liquid Mixtures of Trichloroethylene and Tetrachloroethylene with Some Polar and Nonpolar Solvents
dvisc	0.0006040	Paxs	Densities and Viscosities for the Ternary Systems of Methyl tert-Butyl Ether + Methanol + Benzene and Methyl tert-Butyl Ether + Methanol + Toluene and Their Sub-binary Systems at 298.15 K
fll	1.30	% in Air	KDB
flu	7.90	% in Air	KDB
fpo	262.04	K	KDB
gf	129.70	kJ/mol	KDB
gyrad	3.0040		KDB
hcg	3267.62	kJ/mol	KDB
hcn	3135.573	kJ/mol	KDB
hf	82.98	kJ/mol	KDB
hf	82.80	kJ/mol	NIST Webbook
hf	82.90 ± 0.90	kJ/mol	NIST Webbook
hf	79.90	kJ/mol	NIST Webbook
hf	82.93 ± 0.50	kJ/mol	NIST Webbook
hfl	48.95 ± 0.54	kJ/mol	NIST Webbook
hfl	49.00 ± 0.90	kJ/mol	NIST Webbook
hfl	46.00	kJ/mol	NIST Webbook
hfl	49.04 ± 0.50	kJ/mol	NIST Webbook
hfus	5.73	kJ/mol	Joback Method
hsub	44.40	kJ/mol	NIST Webbook
hvap	30.56	kJ/mol	Joback Method
ie	9.80 ± 0.10	eV	NIST Webbook
ie	9.25 ± 0.01	eV	NIST Webbook
ie	9.25 ± 0.00	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.20	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.24 ± 0.01	eV	NIST Webbook
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ie	9.24	eV	NIST Webbook
ie	9.24 ± 0.01	eV	NIST Webbook

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ie	9.24	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.25 ± 0.01	eV	NIST Webbook
ie	9.24 ± 0.01	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.24 ± 0.00	eV	NIST Webbook
ie	9.36 ± 0.05	eV	NIST Webbook
ie	9.25 ± 0.01	eV	NIST Webbook
ie	9.24 ± 0.01	eV	NIST Webbook
ie	9.27	eV	NIST Webbook
ie	9.26 ± 0.06	eV	NIST Webbook
ie	9.20 ± 0.10	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
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ie	9.24	eV	NIST Webbook
ie	9.22	eV	NIST Webbook
ie	9.25 ± 0.02	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
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ie	9.25	eV	NIST Webbook
ie	9.44	eV	NIST Webbook
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ie	9.24	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
ie	9.20 ± 0.04	eV	NIST Webbook
ie	9.25 ± 0.07	eV	NIST Webbook
ie	9.20	eV	NIST Webbook
log10ws	-1.64		Aqueous Solubility Prediction Method
log10ws	-1.64		Estimated Solubility Method
logp	1.687		Crippen Method
mcvol	71.640	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=2)		KDB
pc	6120.00 ± 709.28	kPa	NIST Webbook
pc	4895.00 ± 6.00	kPa	NIST Webbook
pc	4884.00 ± 20.00	kPa	NIST Webbook
pc	4900.00 ± 10.00	kPa	NIST Webbook
pc	4894.00 ± 10.00	kPa	NIST Webbook
pc	4875.75 ± 30.00	kPa	NIST Webbook
pc	4898.00 ± 2.00	kPa	NIST Webbook
pc	4897.00 ± 10.00	kPa	NIST Webbook
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pc	4936.65 ± 55.15	kPa	NIST Webbook
pc	4853.47 ± 50.66	kPa	NIST Webbook
pc	4895.00	kPa	KDB
pc	4875.00 ± 27.58	kPa	NIST Webbook
pc	4930.90 ± 40.00	kPa	NIST Webbook
pc	4852.30 ± 53.33	kPa	NIST Webbook
pc	5020.00 ± 101.33	kPa	NIST Webbook
pc	4910.00 ± 4.90	kPa	NIST Webbook
pc	4852.27 ± 39.99	kPa	NIST Webbook
pc	4898.00 ± 10.13	kPa	NIST Webbook
rhoc	304.48 ± 3.91	kg/m3	NIST Webbook
rhoc	296.98 ± 7.81	kg/m3	NIST Webbook

rhoc	304.40 ± 3.91	kg/m3	NIST Webbook
rhoc	303.85 ± 4.69	kg/m3	NIST Webbook
rhoc	274.95 ± 1.48	kg/m3	NIST Webbook
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vols	0.00	m3/kg	PVT Relationships of Binary Mixtures of Indole with 2-Methylnaphthalene and Biphenyl at 333.15 K and Pressures up to 270 MPa
zc	0.2681520		KDB
zra	0.27		KDB

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Property code	Value	Unit	Temperature [K]	Source
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cpg	132.94 ± 0.08	J/molxK	473.15	NIST Webbook
cpg	132.42	J/molxK	471.10	NIST Webbook
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cpl	134.60	J/molxK	293.00	NIST Webbook
cpl	130.00	J/molxK	298.00	NIST Webbook
cpl	135.40	J/molxK	298.00	NIST Webbook
cpl	135.90	J/molxK	298.00	NIST Webbook
cpl	135.90	J/molxK	298.15	NIST Webbook
cpl	134.30	J/molxK	298.00	NIST Webbook
cpl	135.70	J/molxK	298.15	NIST Webbook
cpl	135.76	J/molxK	298.15	NIST Webbook
cpl	135.76	J/molxK	298.15	NIST Webbook
cpl	135.60	J/molxK	298.15	NIST Webbook
cpl	135.90	J/molxK	298.15	NIST Webbook
cpl	135.61	J/molxK	298.15	NIST Webbook
cpl	135.90	J/molxK	298.15	NIST Webbook
cpl	133.60	J/molxK	293.15	NIST Webbook

cpl	135.60	J/molxK	298.15	NIST Webbook
cpl	135.74	J/molxK	298.15	NIST Webbook
cpl	135.70	J/molxK	298.15	NIST Webbook
cpl	134.98	J/molxK	298.00	NIST Webbook
cps	118.40	J/molxK	273.00	NIST Webbook
cps	47.86	J/molxK	90.00	NIST Webbook
cps	97.90	J/molxK	223.90	NIST Webbook
dvisc	0.0004970	Paxs	313.15	Density and Viscosity of Propyl Formate + Aromatic Hydrocarbons at T = (303.15, 308.15, and 313.15) K
dvisc	0.0005340	Paxs	308.15	Physical Properties of Binary Mixtures of Ethyl Formate with Benzene, Isopropyl Benzene, Isobutyl Benzene, and Butylbenzene at (303.15, 308.15, and 313.15) K
dvisc	0.0005690	Paxs	303.15	Physical Properties of Binary Mixtures of Ethyl Formate with Benzene, Isopropyl Benzene, Isobutyl Benzene, and Butylbenzene at (303.15, 308.15, and 313.15) K
dvisc	0.0004660	Paxs	318.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K
dvisc	0.0005330	Paxs	308.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K

dvisc	0.0006030	Paxs	298.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K
dvisc	0.0003932	Paxs	333.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0004145	Paxs	328.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0004397	Paxs	323.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0004714	Paxs	318.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K

dvisc	0.0005001	Paxs	313.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0005232	Paxs	308.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0005640	Paxs	303.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0003540	Paxs	343.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures
dvisc	0.0003890	Paxs	333.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures
dvisc	0.0004360	Paxs	323.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures

dvisc	0.0005620	Paxs	303.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures
dvisc	0.0005710	Paxs	303.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K
dvisc	0.0006040	Paxs	298.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K
dvisc	0.0006480	Paxs	293.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K

dvisc	0.0007090	Paxs	288.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K
dvisc	0.0004362	Paxs	323.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0005612	Paxs	303.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0006038	Paxs	298.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure

dvisc	0.0004970	Paxs	313.15	Physical Properties of Binary Mixtures of Ethyl Formate with Benzene, Isopropyl Benzene, Isobutyl Benzene, and Butylbenzene at (303.15, 308.15, and 313.15) K
dvisc	0.0005690	Paxs	303.15	Density and Viscosity of Propyl Formate + Aromatic Hydrocarbons at T = (303.15, 308.15, and 313.15) K
dvisc	0.0005340	Paxs	308.15	Density and Viscosity of Propyl Formate + Aromatic Hydrocarbons at T = (303.15, 308.15, and 313.15) K
dvisc	0.0005260	Paxs	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for $C_mH_{2m+1}(OCH_2CH_2)_nOH$ (m) 1 or 2 or 4 and n) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane

dvisc	0.0006020	Paxs	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for $\text{C}_m\text{H}_{2m+1}(\text{OCH}_2\text{CH}_2)_n\text{OH}$ (m) 1 or 2 or 4 and n) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane
dvisc	0.0005310	Paxs	308.15	Densities, Viscosities, and Thermodynamic Properties of (N,N-Dimethylformamide + Benzene + Chlorobenzene) Ternary Mixtures at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0005680	Paxs	303.15	Densities, Viscosities, and Thermodynamic Properties of (N,N-Dimethylformamide + Benzene + Chlorobenzene) Ternary Mixtures at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0006030	Paxs	298.15	Densities, Viscosities, and Thermodynamic Properties of (N,N-Dimethylformamide + Benzene + Chlorobenzene) Ternary Mixtures at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0006010	Paxs	298.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures

dvisc	0.0004360	Paxs	323.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0004940	Paxs	313.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0004942	Paxs	313.15	Viscometric and Volumetric Properties of 10 Regular Binary Systems at 308.15 K and 313.15 K
dvisc	0.0005630	Paxs	303.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0006010	Paxs	298.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0003450	Paxs	343.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure

dvisc	0.0003880	Paxs	333.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0004360	Paxs	323.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0004930	Paxs	313.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0005610	Paxs	303.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0004670	Paxs	318.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol, and 2-methyl-2-propanol at different temperatures

dvisc	0.0005395	Paxs	308.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol, and 2-methyl-2-propanol at different temperatures
dvisc	0.0006025	Paxs	298.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol, and 2-methyl-2-propanol at different temperatures
dvisc	0.0005000	Paxs	313.15	Densities, Viscosities, and Thermodynamic Properties of (N,N-Dimethylformamide + Benzene + Chlorobenzene) Ternary Mixtures at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0005272	Paxs	308.15	Viscometric and Volumetric Properties of 10 Regular Binary Systems at 308.15 K and 313.15 K
dvisc	0.0004930	Paxs	313.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures
hfust	9.87	kJ/mol	278.69	NIST Webbook
hfust	9.87	kJ/mol	278.70	NIST Webbook
hfust	9.30	kJ/mol	279.10	NIST Webbook
hfust	8.95	kJ/mol	278.80	NIST Webbook
hfust	9.94	kJ/mol	278.60	NIST Webbook
hfust	9.80	kJ/mol	278.60	NIST Webbook
hfust	9.88	kJ/mol	278.55	NIST Webbook
hfust	10.00	kJ/mol	278.64	NIST Webbook

hfust	9.92	kJ/mol	278.65	NIST Webbook
hsubt	45.10	kJ/mol	278.00	NIST Webbook
hsubt	53.90 ± 0.80	kJ/mol	193.00	NIST Webbook
hsubt	41.70	kJ/mol	265.50	NIST Webbook
hsubt	49.40 ± 0.40	kJ/mol	193.00	NIST Webbook
hsubt	45.20	kJ/mol	251.00	NIST Webbook
hsubt	45.60	kJ/mol	244.50	NIST Webbook
hsubt	44.10	kJ/mol	261.00	NIST Webbook
hsubt	43.10	kJ/mol	229.00	NIST Webbook
hsubt	44.60	kJ/mol	279.00	NIST Webbook
hsubt	46.60	kJ/mol	266.50	NIST Webbook
hsubt	38.00	kJ/mol	303.00	NIST Webbook
hsubt	44.60	kJ/mol	273.00	NIST Webbook
hsubt	43.30	kJ/mol	226.00	NIST Webbook
hvapt	31.50	kJ/mol	387.50	NIST Webbook
hvapt	31.40 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	31.80 ± 0.10	kJ/mol	333.00	NIST Webbook
hvapt	32.20 ± 0.10	kJ/mol	328.00	NIST Webbook
hvapt	30.90 ± 0.10	kJ/mol	353.00	NIST Webbook
hvapt	33.00 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	32.60 ± 0.40	kJ/mol	313.00	NIST Webbook
hvapt	30.20	kJ/mol	366.00	NIST Webbook
hvapt	30.50	kJ/mol	361.00	NIST Webbook
hvapt	30.80	kJ/mol	352.00	NIST Webbook
hvapt	30.30	kJ/mol	531.50	NIST Webbook
hvapt	30.20	kJ/mol	461.00	NIST Webbook
hvapt	32.50 ± 0.50	kJ/mol	328.00	NIST Webbook
hvapt	31.00	kJ/mol	350.00	NIST Webbook
hvapt	31.60 ± 0.40	kJ/mol	345.00	NIST Webbook
hvapt	34.10	kJ/mol	319.00	NIST Webbook
hvapt	34.10	kJ/mol	293.00	NIST Webbook
hvapt	34.10	kJ/mol	318.00	NIST Webbook
hvapt	31.20	kJ/mol	294.00	NIST Webbook
hvapt	34.10	kJ/mol	321.00	NIST Webbook
hvapt	34.40	kJ/mol	328.00	NIST Webbook
hvapt	35.30	kJ/mol	343.00	NIST Webbook
hvapt	30.76	kJ/mol	353.30	KDB
hvapt	33.25	kJ/mol	298.00	Enthalpies of Vaporization and Vapor Pressures of Some Deuterated Hydrocarbons. Liquid-Vapor Pressure Isotope Effects
hvapt	33.40	kJ/mol	335.50	NIST Webbook

hvapt	33.20	kJ/mol	325.00	NIST Webbook
hvapt	35.60	kJ/mol	285.50	NIST Webbook
hvapt	34.50	kJ/mol	310.50	NIST Webbook
hvapt	33.40	kJ/mol	307.00	NIST Webbook
hvapt	33.10	kJ/mol	314.00	NIST Webbook
hvapt	32.40	kJ/mol	324.00	NIST Webbook
hvapt	31.90	kJ/mol	332.00	NIST Webbook
hvapt	31.40	kJ/mol	344.00	NIST Webbook
hvapt	30.60	kJ/mol	353.00	NIST Webbook
hvapt	33.50	kJ/mol	336.50	NIST Webbook
hvapt	30.72	kJ/mol	353.30	NIST Webbook
psub	1.23	kPa	260.68	Recommended sublimation pressure and enthalpy of benzene
psub	1.23	kPa	260.68	Recommended sublimation pressure and enthalpy of benzene
psub	1.23	kPa	260.68	Recommended sublimation pressure and enthalpy of benzene
psub	1.00	kPa	258.16	Recommended sublimation pressure and enthalpy of benzene
psub	1.00	kPa	258.16	Recommended sublimation pressure and enthalpy of benzene
psub	1.00	kPa	258.16	Recommended sublimation pressure and enthalpy of benzene
psub	0.81	kPa	255.67	Recommended sublimation pressure and enthalpy of benzene
psub	0.81	kPa	255.67	Recommended sublimation pressure and enthalpy of benzene
psub	0.65	kPa	253.17	Recommended sublimation pressure and enthalpy of benzene

psub	0.65	kPa	253.17	Recommended sublimation pressure and enthalpy of benzene
psub	0.65	kPa	253.17	Recommended sublimation pressure and enthalpy of benzene
psub	0.53	kPa	250.68	Recommended sublimation pressure and enthalpy of benzene
psub	0.10	kPa	233.20	Recommended sublimation pressure and enthalpy of benzene
psub	0.10	kPa	233.20	Recommended sublimation pressure and enthalpy of benzene
psub	0.10	kPa	233.20	Recommended sublimation pressure and enthalpy of benzene
psub	0.13	kPa	235.70	Recommended sublimation pressure and enthalpy of benzene
psub	0.13	kPa	235.70	Recommended sublimation pressure and enthalpy of benzene
psub	0.13	kPa	235.70	Recommended sublimation pressure and enthalpy of benzene
psub	0.16	kPa	238.21	Recommended sublimation pressure and enthalpy of benzene
psub	0.16	kPa	238.21	Recommended sublimation pressure and enthalpy of benzene
psub	0.16	kPa	238.21	Recommended sublimation pressure and enthalpy of benzene

psub	0.21	kPa	240.70	Recommended sublimation pressure and enthalpy of benzene
psub	0.21	kPa	240.70	Recommended sublimation pressure and enthalpy of benzene
psub	0.21	kPa	240.70	Recommended sublimation pressure and enthalpy of benzene
psub	0.27	kPa	243.20	Recommended sublimation pressure and enthalpy of benzene
psub	0.27	kPa	243.20	Recommended sublimation pressure and enthalpy of benzene
psub	0.27	kPa	243.20	Recommended sublimation pressure and enthalpy of benzene
psub	0.34	kPa	245.68	Recommended sublimation pressure and enthalpy of benzene
psub	0.34	kPa	245.68	Recommended sublimation pressure and enthalpy of benzene
psub	0.34	kPa	245.68	Recommended sublimation pressure and enthalpy of benzene
psub	0.42	kPa	248.18	Recommended sublimation pressure and enthalpy of benzene
psub	0.42	kPa	248.18	Recommended sublimation pressure and enthalpy of benzene
psub	0.42	kPa	248.18	Recommended sublimation pressure and enthalpy of benzene

psub	0.53	kPa	250.68	Recommended sublimation pressure and enthalpy of benzene
psub	0.53	kPa	250.68	Recommended sublimation pressure and enthalpy of benzene
psub	0.81	kPa	255.67	Recommended sublimation pressure and enthalpy of benzene
pvap	12.70	kPa	298.15	Thermodynamic properties of mixtures containing ionic liquids Vapor pressures and activity coefficients of n-alcohols and benzene in binary mixtures with 1-methyl-3-butyl-imidazolium bis(trifluoromethyl-sulfonyl) imide
pvap	15.92	kPa	303.15	Thermodynamic properties of mixtures containing ionic liquids Vapor pressures and activity coefficients of n-alcohols and benzene in binary mixtures with 1-methyl-3-butyl-imidazolium bis(trifluoromethyl-sulfonyl) imide
pvap	19.66	kPa	308.15	Thermodynamic properties of mixtures containing ionic liquids Vapor pressures and activity coefficients of n-alcohols and benzene in binary mixtures with 1-methyl-3-butyl-imidazolium bis(trifluoromethyl-sulfonyl) imide

pvap	24.33	kPa	313.15	Thermodynamic properties of mixtures containing ionic liquids Vapor pressures and activity coefficients of n-alcohols and benzene in binary mixtures with 1-methyl-3-butyl-imidazolium bis(trifluoromethyl-sulfonyl) imide
pvap	40.00	kPa	325.60	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	53.33	kPa	333.56	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	66.66	kPa	340.06	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	79.99	kPa	345.61	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	93.32	kPa	350.50	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components

pvap	52.45	kPa	333.15	Vapor liquid equilibria and density measurement for binary mixtures of toluene, benzene, o-xylene, m-xylene, sulfolane and nonane at 333.15K and 353.15K
pvap	100.00	kPa	353.15	Vapor liquid equilibria and density measurement for binary mixtures of toluene, benzene, o-xylene, m-xylene, sulfolane and nonane at 333.15K and 353.15K
pvap	101.30	kPa	353.30	Isobaric vapor-liquid equilibrium for the binary mixtures of nonane with cyclohexane, toluene, m-xylene, or p-xylene at 101.3 kPa
pvap	62.10	kPa	338.15	Phase equilibria and excess molar enthalpies study of the binary systems (pyrrole + hydrocarbon, or an alcohol) and modeling
pvap	101.33	kPa	353.26	Isobaric vapor-liquid equilibrium for binary system of cinnamaldehyde + benzaldehyde at 10, 20 and 30 kPa
pvap	9.98	kPa	293.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	12.64	kPa	298.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	15.85	kPa	303.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	36.24	kPa	323.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	19.71	kPa	308.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	24.30	kPa	313.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	29.73	kPa	318.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	36.09	kPa	323.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	43.51	kPa	328.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	52.11	kPa	333.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	62.01	kPa	338.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	73.35	kPa	343.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	86.27	kPa	348.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	100.91	kPa	353.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	101.33	kPa	353.15	Phase equilibria of three binary systems containing 2,5-dimethylthiophene and 2-ethylthiophene in hydrocarbons
pvap	205.00	kPa	378.35	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS
pvap	366.00	kPa	401.25	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS
pvap	572.00	kPa	421.85	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS
pvap	778.00	kPa	437.45	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS

pvap	1173.00	kPa	460.35	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS
pvap	1622.00	kPa	480.45	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS
pvap	2183.00	kPa	500.15	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS
pvap	2877.00	kPa	520.05	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS
pvap	12.71	kPa	298.15	(Vapour + liquid) equilibria of (1-butanol + benzene, or toluene, or o-, or m-, or p-xylene) at T = 308.15 K
pvap	39.52	kPa	325.60	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	49.45	kPa	331.70	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts

pvap	69.20	kPa	341.70	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	86.40	kPa	348.15	Phase equilibria and excess molar enthalpies study of the binary systems (pyrrole + hydrocarbon, or an alcohol) and modeling
pvap	101.60	kPa	353.60	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	247.52	kPa	385.30	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	499.10	kPa	415.80	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	101.33	kPa	353.25	Vapor Liquid Equilibrium Data for Binary Systems of N,N-Dimethylacetamide with Cyclohexene, Cyclohexane, and Benzene Separately at Atmospheric Pressure
pvap	15.63	kPa	303.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents

pvap	24.45	kPa	313.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents
pvap	36.60	kPa	323.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents
pvap	53.12	kPa	333.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents
pvap	74.82	kPa	343.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents
pvap	101.30	kPa	353.25	Vapor-Liquid Equilibrium for Binary Systems of Allyl Alcohol + Water and Allyl Alcohol + Benzene at 101.3 kPa
pvap	43.65	kPa	328.15	Vapor Liquid Equilibrium and Excess Enthalpy Data for Systems Containing N,N-Dimethylacetamide

pvap	101.33	kPa	353.27	Isobaric Vapor Liquid Equilibrium for Binary and Ternary Systems of Isoamyl Alcohol + Isoamyl Acetate + Dimethyl Sulfoxide at 101.33 kPa
pvap	137.28	kPa	363.15	Vapor-Liquid Equilibria for Four Binary Systems at 363.15 K: N-Methylformamide + Hexane, + Benzene, + Chlorobenzene, and + Acetonitrile
pvap	24.35	kPa	313.14	Vapor-Liquid Equilibrium for Benzene + 2-Methylpentane and Allyl Alcohol + 1-Propanol
pvap	36.15	kPa	323.14	Vapor-Liquid Equilibrium for Benzene + 2-Methylpentane and Allyl Alcohol + 1-Propanol
pvap	52.17	kPa	333.13	Vapor-Liquid Equilibrium for Benzene + 2-Methylpentane and Allyl Alcohol + 1-Propanol
pvap	379.30	kPa	403.15	Isothermal Vapor-Liquid Equilibrium for Methanol and 2,3-Dimethyl-1-butene at 343.06 K, 353.27 K, 363.19 K, and 372.90 K
pvap	35.47	kPa	323.15	Isothermal Phase Equilibria and Excess Molar Enthalpies for Binary Systems with Dimethyl Ether at 323.15 K

pvap	6.08	kPa	283.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	29.85	kPa	318.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	24.40	kPa	313.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	19.81	kPa	308.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	750.14	kPa	435.40	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	15.93	kPa	303.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures

pvap	12.69	kPa	298.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	10.03	kPa	293.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	7.85	kPa	288.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
rfi	1.50090		293.15	Experimental densities and excess volumes for binary mixtures of (dimethyl sulfoxide + an aromatic hydrocarbon) at temperatures from (293.15 to 353.15) K at atmospheric pressure
rfi	1.49790		298.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures

rfi	1.49620	303.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures
rfi	1.49440	308.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures
rfi	1.49290	313.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures
rfi	1.49110	318.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures
rfi	1.49620	303.15	Volumetric, Viscometric, Ultrasonic, and Refractive Index Properties of Liquid Mixtures of Benzene with Industrially Important Monomers at Different Temperatures
rfi	1.49440	308.15	Volumetric, Viscometric, Ultrasonic, and Refractive Index Properties of Liquid Mixtures of Benzene with Industrially Important Monomers at Different Temperatures

rfi	1.49290	313.15	Volumetric, Viscometric, Ultrasonic, and Refractive Index Properties of Liquid Mixtures of Benzene with Industrially Important Monomers at Different Temperatures
rfi	1.49210	308.15	Topological and thermodynamic investigations of molecular interactions in binary mixtures: Molar excess volumes and molar excess enthalpies
rfi	1.38820	293.10	Liquid liquid equilibria of methylcyclohexane benzene N-formylmorpholine at several temperatures
rfi	1.49810	298.15	Separation of aromatic hydrocarbons from alkanes using ammonium ionic liquid C2NTf2 at T = 298.15K
rfi	1.49785	298.15	Isothermal vapor liquid equilibrium at 323.15K and excess molar volumes and refractive indices at 298.15K for the ternary system propyl vinyl ether + 1-propanol + benzene and its binary sub-systems

rfi	1.49764	298.15	Isothermal vapor-liquid equilibrium at T = 333.15 K and excess volumes and molar refractivity deviation at T = 298.15 K for the ternary mixtures {di-methyl carbonate (DMC) + ethanol + benzene} and {DMC+ ethanol + toluene}
rfi	1.49774	298.15	Experimental data, correlation and prediction of the extraction of benzene from cyclic hydrocarbons using [Epy][ESO4] ionic liquid
rfi	1.50090	293.15	Effect of temperature on the volumetric properties of (cyclohexanone + an aromatic hydrocarbon)
rfi	1.50090	293.15	A study of densities and volumetric properties of binary mixtures containing nitrobenzene at T = (293.15 to 353.15) K
rfi	1.49790	298.15	Excess Molar Volumes of (propiophenone + benzene, or toluene, or ethylbenzene, or butylbenzene) at temperatures 298.15 K and 328.15 K
rfi	1.49792	298.15	KDB
rfi	1.50090	298.15	The volumetric properties of (1,2-propanediol carbonate + benzene, or toluene, or styrene) binary mixtures at temperatures from T = 293.15 K to T = 353.15 K

rfi	1.49692	298.15	Azeotropic behaviour of (benzene + cyclohexane + chlorobenzene) ternary mixture using chlorobenzene as entrainer at 101.3 kPa
rfi	1.49710	298.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K
rfi	1.49360	303.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K
rfi	1.49030	308.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K
rfi	1.50500	288.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K

rfi	1.49790	298.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K
rfi	1.48490	303.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K
rfi	1.50090	293.10	Densities and volumetric properties of N-methyl-2-pyrrolidone with aromatic hydrocarbon at different temperature
rfi	1.49540	303.15	Study of activity coefficients for sodium iodide in (methanol + benzene) system by (vapour + liquid) equilibrium measurements
rfi	1.50090	298.15	Densities and excess volumes of binary mixtures of N,N-dimethylformamide with aromatic hydrocarbon at different temperature
rfi	1.50090	293.10	A study on densities and excess volumes in the (c-butyrolactone + aromatic hydrocarbon) system at various temperatures

rfi	1.50240	293.10	(Liquid + liquid) equilibria of three ternary systems: (heptane + benzene + N-formylmorpholine), (heptane + toluene + N-formylmorpholine), (heptane + xylene + N-formylmorpholine) from T = (298.15 to 353.15) K
rfi	1.50090	298.15	Effects of the presence of ethylacetate or benzene on the densities and volumetric properties of mixture (styrene + N,N-dimethylformamide)
rfi	1.49790	298.15	Excess molar volumes of (octane + benzene, or toluene, or 1,3-xylene, or 1,3,5-trimethylbenzene) at temperatures between (298.15 and 328.15) K
rfi	1.49790	298.15	p, Vm, T) measurements of (octane + benzene) at temperatures from (298.15 to 328.15) K and at pressures up to 40 MPa
rfi	1.49774	298.15	Thermophysical properties of the binary mixtures of 2-methyl-tetrahydrofuran with benzene and halobenzenes
rfi	1.49900	298.15	Liquid-liquid equilibria for mixtures of (Furfural + an Aromatic hydrocarbon + an alkane) at T=298.15 K

rfi	1.50150	293.15	Infinite Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol and Tetraethylene Glycol
rfi	1.50110	293.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Anisole with Benzene, Methylbenzene, Ethylbenzene, Propylbenzene, and Butylbenzene at (293.15 and 303.15) K
rfi	1.49774	298.15	Effect of the Chain Length on the Aromatic Ring in the Separation of Aromatic Compounds from Methylcyclohexane Using the Ionic Liquid 1-Ethyl-3-methylpyridinium Ethylsulfate
rfi	1.49774	298.15	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures
rfi	1.50765	283.15	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures

rfi	1.50110	293.15	Solubilities of 3,9-Dimethyl-3,9-dioxide-2,4,8,10-tetraoxa-3,9-diphosphaspiro[5.5]undecane in Selected Solvents
rfi	1.49470	303.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Anisole with Benzene, Methylbenzene, Ethylbenzene, Propylbenzene, and Butylbenzene at (293.15 and 303.15) K
rfi	1.50110	293.15	Solubilities of Methyldiphenylphosphine Oxide in Selected Solvents
rfi	1.49765	298.15	Isobaric Vapor-Liquid Equilibria for the Binary Systems Benzene + Methyl Ethanoate, Benzene + Butyl Ethanoate, and Benzene + Methyl Heptanoate at 101.31kPa
rfi	1.50110	293.15	Solubilities of Triphenylphosphine Oxide in Selected Solvents
rfi	1.48560	318.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K

rfi	1.48870	313.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.49180	308.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.49490	303.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.49800	298.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K

rfi	1.50110	293.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.48560	318.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.48870	313.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.49180	308.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.49490	303.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.49800	298.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K

rfi	1.50110	293.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.50420	288.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.49790	298.15	Volumetric, Viscometric, Ultrasonic, and Refractive Index Properties of Liquid Mixtures of Benzene with Industrially Important Monomers at Different Temperatures
rfi	1.49740	298.15	Experimental Isobaric Vapor-Liquid Equilibria of Binary Mixtures of 2,2,2-Trifluoroethanol with Benzene or Toluene
rfi	1.50110	293.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K

rfi	1.49764	298.15	Isothermal Vapor-Liquid Equilibrium at 333.15 K, Density, and Refractive Index at 298.15 K for the Ternary Mixture of Dibutyl Ether + Ethanol + Benzene and Binary Subsystems
rfi	1.49774	298.15	Liquid Liquid Extraction of Aromatic Compounds from Cycloalkanes Using 1-Butyl-3-methylimidazolium Methylsulfate Ionic Liquid
rfi	1.49774	298.15	Extraction of Benzene from Aliphatic Compounds Using Commercial Ionic Liquids as Solvents: Study of the Liquid Liquid Equilibrium at T = 298.15 K
rfi	1.49774	298.15	Liquid-Liquid Equilibria of the Ternary Systems of Alkane + Aromatic + 1-Ethylpyridinium Ethylsulfate Ionic Liquid at T = (283.15 and 298.15) K
rfi	1.49774	298.15	Liquid Extraction of Benzene from Its Mixtures Using 1-Ethyl-3-methylimidazolium Ethylsulfate as a Solvent
rfi	1.50110	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents
rfi	1.49774	298.15	Separation of Benzene from Linear Alkanes (C6-C9) Using 1-Ethyl-3-Methylimidazolium Ethylsulfate at T = 298.15 K

rfi	1.49720		298.20	Liquid-Liquid Equilibria for Ternary Mixtures (an Ionic Liquid + Benzene +Heptane or Hexadecane) at T) 298.2 K and Atmospheric Pressure
rfi	1.50420		288.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rhoI	878.23	kg/m3	293.15	Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhoI	824.70	kg/m3	343.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	835.70	kg/m3	333.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K

rhoI	846.50	kg/m3	323.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	857.40	kg/m3	313.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	868.20	kg/m3	303.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	874.16	kg/m3	298.15	Experimental and theoretical study of surface tension of binary mixtures of (n-alkyl acetates + heptane, benzene, and toluene)
rhoI	883.90	kg/m3	288.15	Volumetric properties of binary liquid mixtures: Application of the Prigogine Flory Patterson theory to excess molar volumes of dichloromethane with benzene or toluene
rhoI	876.85	kg/m3	293.15	Volumetric properties of binary liquid mixtures: Application of the Prigogine Flory Patterson theory to excess molar volumes of dichloromethane with benzene or toluene

rhoI	873.36	kg/m3	298.15	Volumetric properties of binary liquid mixtures: Application of the Prigogine Flory Patterson theory to excess molar volumes of dichloromethane with benzene or toluene
rhoI	868.71	kg/m3	303.15	Volumetric properties of binary liquid mixtures: Application of the Prigogine Flory Patterson theory to excess molar volumes of dichloromethane with benzene or toluene
rhoI	873.57	kg/m3	298.15	Evaluation of ionic liquids as solvent for aromatic extraction: Experimental, correlation and COSMO-RS predictions
rhoI	873.45	kg/m3	298.15	Experimental and predicted data of excess molar enthalpies and excess molar volumes for the ternary system (1,3-dichlorobenzene + benzene + 1-chlorohexane) at T = 298.15 K
rhoI	873.57	kg/m3	298.15	(Liquid + liquid) equilibrium at T = 298.15 K for ternary mixtures of alkane + aromatic compounds + imidazolium-based ionic liquids
rhoI	878.89	kg/m3	293.15	Excess heat capacities of mixtures containing 1-methylpyrrolidin-2-one, chlorotoluenes and benzene

rhoI	873.54	kg/m3	298.15	Excess heat capacities of mixtures containing 1-methylpyrrolidin-2-one, chlorotoluenes and benzene	
rhoI	868.20	kg/m3	303.15	Excess heat capacities of mixtures containing 1-methylpyrrolidin-2-one, chlorotoluenes and benzene	
rhoI	873.71	kg/m3	298.15	Determination and correlation of (liquid + liquid) equilibria of ternary and quaternary systems with octane, decane, benzene and [BMpyr][DCA] at T = 298.15 K and atmospheric pressure	
rhoI	878.87	kg/m3	293.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K	
rhoI	868.20	kg/m3	303.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K	

rhoI	873.57	kg/m3	298.15	Measurements and equation-of-state modelling of thermodynamic properties of binary mixtures of 1-butyl-1-methylpyrrolidinium tetracyanoborate ionic liquid with molecular compounds
rhoI	857.44	kg/m3	313.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K
rhoI	846.62	kg/m3	323.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K
rhoI	835.71	kg/m3	333.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K
rhoI	868.30	kg/m3	303.15	Studies of partial molar volumes of alkylamine in non-electrolyte solvents I. Alkylamines in hydrocarbons at 303.15 and 313.15K

rhoI	857.59	kg/m3	313.15	Studies of partial molar volumes of alkylamine in non-electrolyte solvents I. Alkylamines in hydrocarbons at 303.15 and 313.15K
rhoI	868.42	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-propanol + ethyl ethanoate + cyclohexane or benzene at 303.15 K: Experimental data, correlation and prediction by ERAS model
rhoI	873.64	kg/m3	298.15	Excess molar volumes and isentropic compressibilities changes of mixing of tetrahydropyran + benzene + cyclo or n-alkanes ternary mixtures at 308.15 K
rhoI	878.93	kg/m3	293.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	873.62	kg/m3	298.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K

rhoI	868.29	kg/m3	303.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	862.94	kg/m3	308.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	857.58	kg/m3	313.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	852.19	kg/m3	318.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K

rhoI	846.77	kg/m3	323.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	874.00	kg/m3	298.15	Liquid Liquid Equilibrium data for the ternary systems of Water, Isopropyl alcohol, and selected entrainers
rhoI	873.45	kg/m3	298.10	Excess Molar Enthalpies of Propyl Propanoate + 1-Hexanol + Benzene at the Temperatures of 25 :C and 35 :C
rhoI	873.64	kg/m3	298.15	Vapor-Liquid Equilibria and Excess Enthalpies for Binary Systems of Dimethoxymethane with Hydrocarbons
rhoI	876.53	kg/m3	293.20	Isobaric Vapor-Liquid Equilibria for Binary Mixtures of 1,2-Dibromoethane with Benzene, Toluene, Fluorobenzene, and Bromobenzene at Atmospheric Pressure
rhoI	873.58	kg/m3	298.15	Volumetric Properties of the Binary Methanol + Chloroform and Ternary Methanol + Chloroform + Benzene Mixtures at (288.15, 293.15, 298.15, 303.15, 308.15, and 313.15) K

rhoI	875.47	kg/m3	298.15	Calorimetric Study of Nitrile Group-Solvent Interactions and Comparison with Dispersive Quasi-Chemical (DISQUAC) Predictions	
rhoI	868.10	kg/m3	303.15	Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K	
rhoI	857.40	kg/m3	313.15	Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K	
rhoI	846.60	kg/m3	323.15	Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K	
rhoI	873.57	kg/m3	298.15	Excess Molar Volumes of 2,4,6,8-Tetramethylcyclotetrasiloxane with Benzene, Toluene, and Xylene at T = (288.15, 298.15, and 308.15) K	
rhoI	873.54	kg/m3	298.15	Thermodynamic Properties of Ternary Liquid Mixtures Containing o-Chlorotoluene: Excess Molar Volumes and Excess Isentropic Compressibilities	
rhoI	868.20	kg/m3	303.15	Thermodynamic Properties of Ternary Liquid Mixtures Containing o-Chlorotoluene: Excess Molar Volumes and Excess Isentropic Compressibilities	

rhoI	862.84	kg/m3	308.15	Thermodynamic Properties of Ternary Liquid Mixtures Containing o-Chlorotoluene: Excess Molar Volumes and Excess Isentropic Compressibilities
rhoI	873.58	kg/m3	298.15	Excess Enthalpies of Chloroalkylbenzene + Alkylbenzene Mixtures
rhoI	873.11	kg/m3	298.15	Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhoI	867.59	kg/m3	303.15	Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhoI	862.21	kg/m3	308.15	Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhoI	862.87	kg/m3	308.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules

rhoI	856.82	kg/m3	313.15	Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhoI	846.05	kg/m3	323.15	Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhoI	835.76	kg/m3	333.15	Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhoI	824.89	kg/m3	343.15	Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhoI	884.25	kg/m3	288.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K

rhoI	878.92	kg/m3	293.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K
rhoI	878.90	kg/m3	293.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	873.20	kg/m3	298.15	Ternary (liquid + liquid) equilibria for mixtures of 1-hexyl-3-methylimidazolium (tetrafluoroborate or hexafluorophosphate) + benzene + an alkane at T = 298.2 K and p = 0.1 MPa
rhoI	873.71	kg/m3	298.15	Application of the ionic liquid tributylmethylammonium bis(trifluoromethylsulfonyl)imide as solvent for the extraction of benzene from octane and decane at T = 298.15 K and atmospheric pressure
rhoI	873.58	kg/m3	298.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K

rhoI	868.23	kg/m3	303.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K
rhoI	862.87	kg/m3	308.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K
rhoI	857.50	kg/m3	313.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K
rhoI	868.10	kg/m3	303.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K
rhoI	857.40	kg/m3	313.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K

rhoI	846.60	kg/m3	323.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K
rhoI	873.50	kg/m3	298.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes and Aromatic Compounds at T = 313.15 K
rhoI	873.64	kg/m3	298.15	Molar Excess Volumes and Excess Isentropic Compressibilities of {2-Methylaniline (i) + Benzene (j) + Methylbenzene}, {2-Methylaniline (i) + Benzene (j) + 1,2-Dimethylbenzene (k)}, and {2-Methylaniline (i) + Benzene (j) + 1,4-Dimethylbenzene (k)} at T = 308.15 K
rhoI	885.00	kg/m3	289.00	KDB
rhoI	884.25	kg/m3	288.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)

rhoI	878.92	kg/m3	293.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
rhoI	873.58	kg/m3	298.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
rhoI	873.40	kg/m3	298.15	Mutual Solubility of Pyridinium-Based Tetrafluoroborates and Toluene
rhoI	862.87	kg/m3	308.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
rhoI	857.50	kg/m3	313.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)

rhoI	884.30	kg/m3	288.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K
rhoI	878.95	kg/m3	293.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K
rhoI	873.61	kg/m3	298.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K
rhoI	868.26	kg/m3	303.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K

rhoI	862.90	kg/m3	308.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K
rhoI	857.56	kg/m3	313.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K
rhoI	868.23	kg/m3	303.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules
rhoI	873.62	kg/m3	298.15	Topological Investigations of Excess Molar Volumes and Excess Isentropic Compressibilities of Ternary Mixtures Containing Pyrrolidin-2-one at 308.15 K
rhoI	873.66	kg/m3	298.15	Densities, Viscosities, Speeds of Sound, and Refractive Indices of Binary Mixtures of 2-Ethyl-1-hexanol with Benzene and Halobenzenes

rhoI	868.29	kg/m3	303.15	Densities, Viscosities, Speeds of Sound, and Refractive Indices of Binary Mixtures of 2-Ethyl-1-hexanol with Benzene and Halobenzenes
rhoI	862.92	kg/m3	308.15	Densities, Viscosities, Speeds of Sound, and Refractive Indices of Binary Mixtures of 2-Ethyl-1-hexanol with Benzene and Halobenzenes
rhoI	873.60	kg/m3	298.15	Fluid Phase Topology of Benzene + Cyclohexane + 1-Propanol at 101.3 kPa
rhoI	873.55	kg/m3	298.15	Experimental and predicted vapour liquid equilibrium of 1,4-dioxane with cycloalkanes and benzene
rhoI	884.25	kg/m3	288.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules
rhoI	878.92	kg/m3	293.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules
rhoI	873.58	kg/m3	298.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules

rhoI	873.71	kg/m3	298.15	Study of the suitability of two ammonium-based ionic liquids for the extraction of benzene from its mixtures with aliphatic hydrocarbons.
rhoI	873.73	kg/m3	298.15	Liquid liquid equilibria in the ternary systems {hexadecane + BTX aromatics + 2-methoxyethanol or acetonitrile} at 298.15 K
rhoI	873.53	kg/m3	298.15	Phase behaviour of tricyanomethanide-based ionic liquids with alcohols and hydrocarbons
rhoI	862.84	kg/m3	308.15	Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic hydrocarbons
rhoI	868.20	kg/m3	303.15	Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic hydrocarbons
rhoI	873.54	kg/m3	298.15	Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic hydrocarbons
rhoI	873.79	kg/m3	298.15	Liquid-liquid equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, and 318.15) K

rhoI	873.53	kg/m3	298.15	Phase behaviour of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons
rhoI	846.76	kg/m3	323.00	Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K
rhoI	857.57	kg/m3	313.00	Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K
rhoI	868.30	kg/m3	303.00	Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K
rhoI	878.98	kg/m3	293.00	Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K
rhoI	873.95	kg/m3	298.15	Liquid liquid equilibrium of ternary systems 1-butyl-3-methylimidazolium hexafluorophosphate + aromatic + aliphatic
rhoI	857.50	kg/m3	313.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS

rhoI	862.87	kg/m3	308.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS
rhoI	868.23	kg/m3	303.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS
rhoI	873.58	kg/m3	298.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS
rhoI	878.92	kg/m3	293.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS

rhoI	884.25	kg/m3	288.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS
rhoI	873.58	kg/m3	298.15	Thermodynamic study of 1,1,2,2-tetrachloroethane + hydrocarbon mixtures I. Excess and solvation enthalpies
rhoI	873.67	kg/m3	298.10	Excess enthalpies of binary mixtures of 2-ethoxyethanol with four hydrocarbons at 298.15, 308.15, and 318.15K An experimental and theoretical study
rhoI	857.50	kg/m3	313.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules
rhoI	852.23	kg/m3	318.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K

rhoI	868.23	kg/m3	303.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
sfust	35.40	J/molxK	278.69	NIST Webbook
sfust	35.90	J/molxK	278.64	NIST Webbook
sfust	35.50	J/molxK	278.55	NIST Webbook
sfust	35.19	J/molxK	278.60	NIST Webbook
sfust	32.10	J/molxK	278.80	NIST Webbook
sfust	33.30	J/molxK	279.10	NIST Webbook
sfust	35.59	J/molxK	278.65	NIST Webbook
speedsl	1345.47	m/s	288.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}
speedsl	1368.70	m/s	283.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures
speedsl	1298.30	m/s	298.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures
speedsl	1229.50	m/s	313.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures

speedsl	1345.47	m/s	288.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1333.44	m/s	290.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1321.59	m/s	293.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1309.88	m/s	295.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1298.27	m/s	298.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1286.68	m/s	300.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1275.13	m/s	303.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives

speedsl	1263.59	m/s	305.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1252.08	m/s	308.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1240.69	m/s	310.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1229.29	m/s	313.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1217.94	m/s	315.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1206.70	m/s	318.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1195.55	m/s	320.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives

speedsl	1184.63	m/s	323.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1298.00	m/s	298.15	Isentropic Compressibilities Changes of Mixing of Tetrahydropyran and Aromatic Hydrocarbons Ternary Mixtures at 308.15 K
speedsl	1316.50	m/s	293.00	Ultrasonic velocity, viscosity and excess properties of binary mixture of tetrahydrofuran with 1-propanol and 2-propanol
speedsl	1294.00	m/s	298.00	Ultrasonic velocity, viscosity and excess properties of binary mixture of tetrahydrofuran with 1-propanol and 2-propanol
speedsl	1272.80	m/s	303.00	Ultrasonic velocity, viscosity and excess properties of binary mixture of tetrahydrofuran with 1-propanol and 2-propanol
speedsl	1226.50	m/s	313.00	Ultrasonic velocity, viscosity and excess properties of binary mixture of tetrahydrofuran with 1-propanol and 2-propanol
speedsl	1298.20	m/s	298.15	Sound speed and density measurements for tetra-n-butylammonium bromide in benzene and carbon tetrachloride solutions at T = 298.15 K

speedsl	1260.00	m/s	308.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1300.00	m/s	298.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1260.00	m/s	308.15	Densities, Excess Molar Volumes at T = (298.15 to 313.15) K, Speeds of Sound, Excess Isentropic Compressibilities, Relative Permittivities and Deviations in Molar Polarizations at T = (298.15 and 308.15) K for Methyl Methacrylate + 2-Butoxyethanol or + Dibutyl Ether + Benzene, + Toluene and + p-Xylene

speedsl	1299.00	m/s	298.15	Densities, Excess Molar Volumes at T = (298.15 to 313.15) K, Speeds of Sound, Excess Isentropic Compressibilities, Relative Permittivities and Deviations in Molar Polarizations at T = (298.15 and 308.15) K for Methyl Methacrylate + 2-Butoxyethanol or + Dibutyl Ether + Benzene, + Toluene and + p-Xylene
speedsl	1184.50	m/s	323.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K
speedsl	1207.00	m/s	318.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K
speedsl	1229.80	m/s	313.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K

speedsl	1252.80	m/s	308.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K
speedsl	1276.00	m/s	303.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K
speedsl	1299.30	m/s	298.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K
speedsl	1322.70	m/s	293.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K
speedsl	1184.47	m/s	323.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1207.04	m/s	318.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K

speedsl	1229.76	m/s	313.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1252.76	m/s	308.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1275.96	m/s	303.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1299.33	m/s	298.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1322.72	m/s	293.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1207.80	m/s	318.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods

speedsl	1229.30	m/s	313.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods
speedsl	1252.40	m/s	308.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods
speedsl	1275.70	m/s	303.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods
speedsl	1299.50	m/s	298.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods
speedsl	1324.40	m/s	293.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods

speedsl	1298.00	m/s	298.15	Thermodynamic and topological investigations of molecular interactions in binary and ternary mixtures containing 1-methyl pyrrolidin-2-one at T = 308.15 K
speedsl	1184.63	m/s	323.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}
speedsl	1298.27	m/s	298.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}
speedsl	1259.00	m/s	308.15	Thermodynamic and topological investigations of molecular interactions in binary and ternary mixtures containing 1-methyl pyrrolidin-2-one at T = 308.15 K
srf	0.03	N/m	293.20	KDB
srf	0.03	N/m	280.25	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	283.13	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	285.64	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	288.11	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene

srf	0.03	N/m	290.58	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	293.08	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	295.46	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	298.09	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	300.41	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	303.24	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	306.00	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	308.05	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	310.32	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene
srf	0.03	N/m	313.44	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene

srf	0.03	N/m	293.15	Investigation of Surface Properties and Solubility of 1-Vinyl-3-alkyl/Esterimidazolium Halide Ionic Liquids by Density Functional Methods
tcondl	0.15	W/m×K	281.18	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.15	W/m×K	281.49	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.15	W/m×K	281.76	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	295.92	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.11	W/m×K	392.16	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K
tcondl	0.14	W/m×K	296.53	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	301.25	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	301.59	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	301.87	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.13	W/m×K	319.14	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	319.49	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	319.79	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	302.75	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K
tcondl	0.13	W/m×K	332.54	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K
tcondl	0.12	W/m×K	362.39	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K

tcondl	0.14	W/m×K	296.25	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
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Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	353.35	K	96.60	Low cost apparatus for rapid boiling point determination of small air sensitive samples under inert atmosphere
tfp	351.25	K	300000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	293.15	K	53620.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction
tfp	303.15	K	92220.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction

tfp	313.15	K	133290.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction
tfp	323.15	K	176820.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction
tfp	333.15	K	222810.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction
tfp	343.15	K	271270.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction
tfp	353.15	K	322200.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction
tfp	306.44	K	100000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa

tfp	329.93	K	200000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	278.94	K	100.00	Activity coefficient at infinite dilution, azeotropic data, excess enthalpies and solid liquid-equilibria for binary systems of alkanes and aromatics with esters
tfp	370.85	K	400000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	389.07	K	500000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	406.15	K	600000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa

tfp	422.25	K	700000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	437.52	K	800000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	452.06	K	900000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	465.96	K	1000000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	538.73	K	1500000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa

tfp	584.85	K	2000000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	625.73	K	2500000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	663.67	K	3000000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.36756e+01
Coeff. B	-2.51081e+03
Coeff. C	-7.60040e+01
Temperature range (K), min.	263.55
Temperature range (K), max.	376.19

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	7.11072e+01
Coeff. B	-6.28104e+03

Coeff. C	-8.43361e+00
Coeff. D	6.19841e-06
Temperature range (K), min.	278.68
Temperature range (K), max.	562.16

Datasets

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
313.20	690.00	0.0004790
313.20	5000.00	0.0005000
313.20	10000.00	0.0005240
313.20	20000.00	0.0005740
313.20	30000.00	0.0006250
313.20	40000.00	0.0006750
313.20	50000.00	0.0007250
313.20	60000.00	0.0007740
333.20	690.00	0.0003870
333.20	5000.00	0.0004040
333.20	10000.00	0.0004240
333.20	20000.00	0.0004660
333.20	30000.00	0.0005090
333.20	40000.00	0.0005530
333.20	50000.00	0.0005970
333.20	60000.00	0.0006410
353.20	690.00	0.0003170
353.20	5000.00	0.0003310
353.20	10000.00	0.0003470
353.20	20000.00	0.0003800
353.20	30000.00	0.0004150
353.20	40000.00	0.0004510
353.20	50000.00	0.0004890
353.20	60000.00	0.0005260
373.20	690.00	0.0002690
373.20	5000.00	0.0002790
373.20	10000.00	0.0002910
373.20	20000.00	0.0003160
373.20	30000.00	0.0003440

373.20	40000.00	0.0003720
373.20	50000.00	0.0004020
373.20	60000.00	0.0004340
393.20	690.00	0.0002390
393.20	5000.00	0.0002460
393.20	10000.00	0.0002550
393.20	20000.00	0.0002730
393.20	30000.00	0.0002940
393.20	40000.00	0.0003150
393.20	50000.00	0.0003390
393.20	60000.00	0.0003640

Reference

<https://www.doi.org/10.1016/j.fluid.2007.08.010>

Temperature, K	Pressure, kPa	Viscosity, Pa*s
303.15	101.30	0.0005390

Reference

<https://www.doi.org/10.1021/je034204h>

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
293.00	2100.00	877.4
293.00	3100.00	878.1
293.00	4100.00	878.8
293.00	5000.00	879.6
293.00	10100.00	883.4
293.00	20000.00	890.4
293.00	30000.00	896.9
293.00	40000.00	902.9
293.00	50000.00	908.6
293.00	60000.00	914.0
293.00	70000.00	919.6
313.00	2100.00	857.0
313.00	3100.00	857.8
313.00	4100.00	858.7
313.00	5000.00	859.6
313.00	10100.00	863.9
313.00	20000.00	871.5
313.00	30000.00	878.7

313.00	40000.00	885.2
313.00	50000.00	891.6
313.00	60000.00	897.5
313.00	70000.00	902.9
333.00	2100.00	835.1
333.00	3100.00	836.0
333.00	4100.00	837.0
333.00	5000.00	838.0
333.00	10100.00	842.7
333.00	20000.00	851.8
333.00	30000.00	859.4
333.00	40000.00	867.0
333.00	50000.00	874.2
333.00	60000.00	880.8
333.00	70000.00	886.7
353.00	2100.00	813.1
353.00	3100.00	814.2
353.00	4100.00	815.4
353.00	5000.00	816.5
353.00	10100.00	822.3
353.00	20000.00	832.3
353.00	30000.00	841.2
353.00	40000.00	849.5
353.00	50000.00	857.0
353.00	60000.00	864.3
353.00	70000.00	871.2
373.00	2100.00	790.7
373.00	3100.00	792.1
373.00	4100.00	793.4
373.00	5000.00	794.7
373.00	10100.00	801.4
373.00	20000.00	812.9
373.00	30000.00	823.1
373.00	40000.00	832.3
373.00	50000.00	840.7
373.00	60000.00	848.2
373.00	70000.00	855.7
393.00	2100.00	767.6
393.00	3100.00	769.4
393.00	4100.00	770.9
393.00	5000.00	772.5
393.00	10100.00	780.0
393.00	20000.00	793.0
393.00	30000.00	804.5

393.00	40000.00	814.6
393.00	50000.00	824.0
393.00	60000.00	832.6
393.00	70000.00	841.0
413.00	2100.00	743.0
413.00	3100.00	745.1
413.00	4100.00	747.0
413.00	5000.00	748.8
413.00	10100.00	758.0
413.00	20000.00	773.2
413.00	30000.00	786.2
413.00	40000.00	797.5
413.00	50000.00	807.8
413.00	60000.00	817.2
413.00	70000.00	825.8
433.00	2100.00	716.7
433.00	3100.00	719.4
433.00	4100.00	721.8
433.00	5000.00	724.0
433.00	10100.00	735.4
433.00	20000.00	753.0
433.00	30000.00	767.8
433.00	40000.00	780.3
433.00	50000.00	791.6
433.00	60000.00	801.7
433.00	70000.00	811.0
448.00	2100.00	696.0
448.00	3100.00	699.2
448.00	4100.00	702.1
448.00	5000.00	704.8
448.00	10100.00	717.8
448.00	20000.00	738.0
448.00	30000.00	754.2
448.00	40000.00	767.8
448.00	50000.00	779.8
448.00	60000.00	790.6
448.00	70000.00	800.3
468.00	2100.00	666.9
468.00	3100.00	670.7
468.00	4100.00	674.3
468.00	5000.00	677.8
468.00	10100.00	693.2
468.00	20000.00	717.0
468.00	30000.00	735.1

468.00	40000.00	750.3
468.00	50000.00	763.6
468.00	60000.00	775.5
468.00	70000.00	786.1

Reference

<https://www.doi.org/10.1016/j.fluid.2016.09.021>

Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
283.15	101.00	1371.6
283.15	1112.00	1376.8
283.15	2281.00	1382.4
283.15	4616.00	1393.2
283.15	6766.00	1403.3
283.15	9100.00	1413.6
283.15	11628.00	1424.5
283.15	14278.00	1436.0
283.15	15957.00	1443.4
283.15	18556.00	1454.0
283.15	20823.00	1463.0
283.15	23405.00	1473.4
298.15	101.00	1299.9
298.15	888.00	1305.0
298.15	1246.00	1305.8
298.15	2254.00	1311.8
298.15	2506.00	1312.2
298.15	4580.00	1322.5
298.15	4719.00	1323.9
298.15	6991.00	1334.4
298.15	7131.00	1335.5
298.15	9327.00	1346.2
298.15	9335.00	1346.2
298.15	9408.00	1346.0
298.15	11563.00	1355.8
298.15	11640.00	1357.0
298.15	14137.00	1368.5
298.15	14317.00	1368.6
298.15	15927.00	1375.9
298.15	16524.00	1379.1
298.15	18655.00	1388.6

298.15	18844.00	1389.0
298.15	20826.00	1398.1
298.15	21001.00	1398.6
298.15	23151.00	1407.9
298.15	23834.00	1410.7
298.15	25699.00	1418.5
298.15	26172.00	1420.5
298.15	28369.00	1428.5
298.15	101.00	1300.2
313.15	101.00	1230.8
313.15	2047.00	1241.3
313.15	3268.00	1247.8
313.15	5111.00	1257.8
313.15	7199.00	1268.7
313.15	9383.00	1280.0
313.15	11613.00	1291.3
313.15	14139.00	1303.7
313.15	16386.00	1314.6
313.15	18686.00	1325.5
313.15	21242.00	1337.2
313.15	23254.00	1346.4
313.15	24384.00	1351.3
313.15	25607.00	1357.2
313.15	25608.00	1357.3
313.15	28210.00	1368.6
333.15	101.00	1142.4
333.15	1260.00	1148.0
333.15	2426.00	1155.0
333.15	5026.00	1170.5
333.15	7135.00	1182.9
333.15	9195.00	1194.5
333.15	11729.00	1208.4
333.15	14011.00	1220.6
333.15	16310.00	1232.7
333.15	18687.00	1244.8
333.15	20059.00	1251.8
333.15	21112.00	1257.2
333.15	23196.00	1267.4
333.15	25517.00	1278.7
333.15	28165.00	1287.7

Reference

<https://www.doi.org/10.1016/j.jct.2004.04.013>

Temperature, K

Pressure, kPa

Frequency, MHz

Speed of sound, m/s

303.15	101.33	2.0	1257.0
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Reference <https://www.doi.org/10.1016/j.jct.2004.12.001>

Pressure, kPa	Temperature, K	Speed of sound, m/s
29815.10	283.21	1498.11
24857.00	283.20	1479.03
20203.80	283.20	1460.21
15331.80	283.20	1439.87
10233.80	283.20	1418.25
5280.10	283.20	1395.99
102.10	283.20	1372.03
30106.10	298.20	1436.88
25017.80	298.20	1415.76
20104.10	298.20	1394.27
14866.50	298.20	1371.03
10068.60	298.20	1349.48
5421.70	298.20	1326.99
84.20	298.20	1299.74
29980.00	313.20	1375.67
25204.40	313.20	1354.82
20194.50	313.20	1332.15
15331.60	313.20	1309.02
10140.00	313.20	1283.5
5536.50	313.20	1259.76
61.20	313.20	1230.41
30145.60	333.21	1299.17
24756.40	333.21	1273.95
19600.70	333.21	1248.51
15038.40	333.21	1225.05
10149.20	333.21	1198.3
5378.80	333.21	1171.44
153.70	333.21	1139.68
30063.00	353.21	1225.96
24679.70	353.21	1198.74
19917.50	353.20	1173.19
15092.20	353.20	1146.64
10006.90	353.21	1116.2
5094.90	353.21	1084.94
172.30	353.21	1052.25

Reference <https://www.doi.org/10.1021/je501065g>

Sources

[illegible]

<https://www.doi.org/10.1021/je025625m>

<https://www.doi.org/10.1021/je4001894>

<https://www.doi.org/10.1016/j.jct.2013.08.022>

<https://www.doi.org/10.1021/je900460m>

<https://www.doi.org/10.1016/j.jct.2007.01.004>

<https://www.doi.org/10.1016/j.fluid.2006.10.013>

<https://www.doi.org/10.1021/je901071x>

<https://www.doi.org/10.1021/je600578u>

<https://www.doi.org/10.1016/j.jct.2005.02.012>

<https://www.doi.org/10.1021/je400635d>

<https://www.doi.org/10.1016/j.fluid.2012.09.013>

<https://www.doi.org/10.1016/j.ijct.2014.12.031>

<https://www.doi.org/10.1021/je5004719>

<https://www.doi.org/10.1021/je030122h>

<https://www.doi.org/10.1021/je400076x>

<https://www.doi.org/10.1021/je050488p>

<https://www.doi.org/10.1016/j.ict.2014.12.023>

<https://www.doi.org/10.1021/je700591h>

<https://www.doi.org/10.1016/j.fluid.2013.12.002>

<https://www.doi.org/10.1016/j.ijct.2006.07.022>

<https://www.doi.org/10.1016/j.ijct.2012.03.005>

<https://www.doi.org/10.1016/j.fluid.2013.01.027>

<https://www.doi.org/10.1016/j.ijct.2005.03.019>

<https://www.doi.org/10.1016/j.fluid.2005.04.021>

<https://www.doi.org/10.1016/j.ijct.2018.05.017>

<https://www.doi.org/10.1016/j.fluid.2007.06.001>

<https://www.doi.org/10.1016/j.fluid.2017.04.008>

<https://www.doi.org/10.1007/s10765-010-0768-y>

<https://www.doi.org/10.1016/j.tsc.2006.03.012>

<https://www.doi.org/10.1016/j.ijct.2011.05.022>

<https://www.doi.org/10.1021/acs.iced.7b00206>

sphoramidate
<https://www.doi.org/10.1016/j.ijct.2018.05.003>

<https://www.doi.org/10.1016/j.tsc.2016.05.011>

<https://www.doi.org/10.1021/ie800579i>

<https://www.doi.org/10.1031/acs.jced.6b00733>

<https://www.doi.org/10.1021/jc9008443>

<https://www.doi.org/10.1016/j.ijet.2012.01.016>

<https://www.doi.org/10.1021/jc060423z>

[illegible]

<https://www.doi.org/10.1021/je034033g>
<https://www.doi.org/10.1016/j.jct.2010.12.021>
<https://www.doi.org/10.1016/j.jct.2004.01.001>
<https://www.doi.org/10.1016/j.fluid.2012.08.004>
<https://www.doi.org/10.1016/j.fluid.2007.07.016>
<https://www.doi.org/10.1021/acs.jced.5b00011>
<https://www.doi.org/10.1016/j.jct.2013.07.004>
<https://www.doi.org/10.1016/j.fluid.2018.06.013>
<https://www.doi.org/10.1021/je100652b>
<https://www.doi.org/10.1021/je7002447>
<https://www.doi.org/10.1021/je034162x>
<https://www.doi.org/10.1021/je800842z>
<https://www.doi.org/10.1016/j.jct.2011.05.009>
<https://www.doi.org/10.1021/je700449z>
<https://www.doi.org/10.1007/s10765-015-1922-3>
<https://www.doi.org/10.1021/je800915d>
<https://www.doi.org/10.1016/j.jct.2010.07.016>
<https://www.doi.org/10.1016/j.jct.2012.08.022>
<https://www.doi.org/10.1021/je6005696>
<https://www.doi.org/10.1021/je500939v>
<https://www.doi.org/10.1021/je900977e>
<https://www.doi.org/10.1016/j.jct.2008.04.002>
<https://www.doi.org/10.1021/je0256481>
<https://www.doi.org/10.1021/je050039p>
<https://www.doi.org/10.1016/j.jct.2009.07.017>
<https://www.doi.org/10.1016/j.jct.2006.12.004>
<https://www.doi.org/10.1021/je060041w>
<https://www.doi.org/10.1016/j.jct.2010.10.003>
<https://www.doi.org/10.1016/j.fluid.2016.07.004>
<https://www.doi.org/10.1016/j.fluid.2013.10.029>
<https://www.doi.org/10.1016/j.jct.2014.12.027>
<https://www.doi.org/10.1021/je700254t>
<https://www.doi.org/10.1007/s10765-010-0861-2>
<https://www.doi.org/10.1016/j.jct.2013.07.011>
<https://www.doi.org/10.1016/j.jct.2005.12.003>
<https://www.doi.org/10.1021/je901065e>
<https://www.doi.org/10.1016/j.jct.2013.01.005>
<https://www.doi.org/10.1021/je0602925>
<https://www.doi.org/10.1016/j.jct.2013.02.006>
<https://www.doi.org/10.1021/je700297c>
<https://www.doi.org/10.1016/j.jct.2014.12.022>
<https://www.doi.org/10.1021/je400412z>
<https://www.doi.org/10.1021/je060033f>

[illegible]

<https://www.doi.org/10.1016/j.jct.2007.02.007>
<https://www.doi.org/10.1021/je0600799>
<https://www.doi.org/10.1021/je200151j>
<https://www.doi.org/10.1021/je0498107>
<https://www.doi.org/10.1016/j.jct.2011.02.012>
<https://www.doi.org/10.1016/j.jct.2013.05.008>
<https://www.doi.org/10.1016/j.jct.2011.11.005>
<https://www.doi.org/10.1016/j.fluid.2013.05.038>
<https://www.doi.org/10.1016/j.fluid.2019.01.028>
<https://www.doi.org/10.1016/j.jct.2006.10.005>
<https://www.doi.org/10.1016/j.jct.2005.03.014>
<https://www.doi.org/10.1021/je9003178>
<https://www.doi.org/10.1021/je7005665>
<https://www.doi.org/10.1021/acs.jced.5b00760>
<https://www.doi.org/10.1016/j.jct.2010.10.026>
<https://www.doi.org/10.1016/j.fluid.2005.10.022>
https://en.wikipedia.org/wiki/Joback_method
<https://www.doi.org/10.1021/je101304x>
<https://www.doi.org/10.1016/j.fluid.2011.10.009>
<https://www.doi.org/10.1021/je800105r>
<https://www.doi.org/10.1016/j.jct.2010.12.019>
<https://www.doi.org/10.1016/j.fluid.2014.03.003>
<https://www.doi.org/10.1021/je030187k>
<https://www.doi.org/10.1016/j.jct.2015.06.003>
<https://www.doi.org/10.1016/j.jct.2017.03.004>
<https://www.doi.org/10.1016/j.fluid.2011.01.025>
<https://www.doi.org/10.1021/je7003885>
<https://www.doi.org/10.1021/je100077z>
<https://www.doi.org/10.1016/j.tca.2008.11.007>
<https://www.doi.org/10.1016/j.jct.2015.05.022>
<https://www.doi.org/10.1021/acs.jced.6b00219>
<https://www.doi.org/10.1021/acs.jced.9b00341>
<https://www.doi.org/10.1021/acs.jced.8b00601>
<https://www.doi.org/10.1016/j.jct.2007.11.002>
<https://www.doi.org/10.1021/je7007268>
<https://www.doi.org/10.1021/je9004189>
<https://www.doi.org/10.1016/j.fluid.2018.06.003>
<https://www.doi.org/10.1021/je300692s>
<https://www.doi.org/10.1016/j.jct.2006.06.005>
<https://www.doi.org/10.1016/j.jct.2015.07.046>
<https://www.doi.org/10.1016/j.fluid.2005.09.010>
<https://www.doi.org/10.1021/acs.jced.7b00538>
<https://www.doi.org/10.1021/je060142u>

[illegible]

<https://www.doi.org/10.1016/j.jct.2012.01.019>
<https://www.doi.org/10.1021/je034203p>
<https://www.doi.org/10.1021/je100410k>
<https://www.doi.org/10.1016/j.fluid.2014.06.020>
<https://www.doi.org/10.1016/j.tca.2009.07.017>
<https://www.doi.org/10.1016/j.jct.2013.05.030>
<https://www.doi.org/10.1021/acs.jced.7b00191>
<https://www.doi.org/10.1016/j.jct.2005.08.018>
<https://www.doi.org/10.1016/j.jct.2009.07.023>
<https://www.doi.org/10.1021/je8006869>
<https://www.doi.org/10.1016/j.fluid.2004.12.005>
<https://www.doi.org/10.1021/acs.jced.6b00970>
<https://www.doi.org/10.1016/j.fluid.2014.06.024>
<https://www.doi.org/10.1021/je050517w>
<https://www.doi.org/10.1016/j.jct.2019.05.011>
<https://www.doi.org/10.1016/j.jct.2013.12.024>
<https://www.doi.org/10.1016/j.tca.2017.05.005>
<https://www.doi.org/10.1021/je500205z>
<https://www.doi.org/10.1021/je300826t>
<https://www.doi.org/10.1016/j.fluid.2013.09.044>
<https://www.doi.org/10.1021/je800676s>
<https://www.doi.org/10.1021/je1000582>
<https://www.doi.org/10.1016/j.jct.2012.08.016>
<https://www.doi.org/10.1016/j.jct.2013.10.038>
<https://www.doi.org/10.1016/j.fluid.2013.05.016>
<https://www.doi.org/10.1021/je800882f>
<https://www.doi.org/10.1016/j.jct.2012.09.017>
<https://www.doi.org/10.1016/j.fluid.2010.05.009>
<https://www.doi.org/10.1021/acs.jced.7b00585>
<https://www.doi.org/10.1016/j.tca.2005.08.034>
<https://www.doi.org/10.1016/j.jct.2013.05.035>
<https://www.doi.org/10.1016/j.jct.2004.11.023>
<https://www.doi.org/10.1016/j.jct.2007.05.005>
<https://www.doi.org/10.1021/je500450w>
<https://www.doi.org/10.1016/j.fluid.2012.09.019>
<https://www.doi.org/10.1016/j.jct.2006.02.001>
<https://www.doi.org/10.1016/j.fluid.2019.03.016>
<https://www.doi.org/10.1016/j.jct.2010.02.006>
<https://www.doi.org/10.1016/j.jct.2015.06.004>
<https://www.doi.org/10.1016/j.fluid.2004.02.021>
<https://www.doi.org/10.1016/j.jct.2011.06.007>
<https://www.doi.org/10.1021/acs.jced.7b00840>
<https://www.doi.org/10.1021/je7002918>

Thermodynamic properties of mixtures containing ionic liquids Vapor pressure and activity coefficients of Refractive index of benzene Binary Systems Sodium Chloride (1) - 1,4-Dioxane Hexane Binary Systems of Acetophenone Benzene and Chloroform with Organic Compounds in Ethylmethylammonium Chloride at Infinite Dilution of Alkanes, Alkenes, and Alkyl Benzenes and volumetric properties of (N-Ethyl-3-morpholine)azepanone Hydroxyaromatics with 1-octanol and 1-octanol with systems of representative compounds of gas chromatograph at 200°C in 1-octanol and 1-octanol for Supercritical fluids for Supercritical fluids Properties of Propyl Propanoate + 1-Hexanol + Benzene at Selected Temperatures of 20-100°C from aromatics in the presence of the {[empty][Tf2N] + [emim][DCA]} ionic liquid mixture;

<https://www.doi.org/10.1016/j.ijct.2015.12.033>

<https://www.doi.org/10.1021/je1001544>

<https://www.doi.org/10.1021/je900689m>

<https://www.doi.org/10.1021/acs.jced.6b00164>

<https://www.doi.org/10.1021/acs.jced.5b00395>

<https://www.doi.org/10.1016/j.ijct.2012.03.015>

<https://www.doi.org/10.1021/je101114r>

<https://www.doi.org/10.1021/acs.iced.5b00542>

<https://www.doi.org/10.1021/ie020145a>

<https://www.doi.org/10.1016/j.ijct.2014.12.005>

<https://www.doi.org/10.1021/ie100081v>

<https://www.doi.org/10.1016/j.ijct.2005.04.010>

<https://www.doi.org/10.1016/j.fluid.2012.10.007>

<https://www.doi.org/10.1016/j.ijct.2004.12.008>

<https://www.doi.org/10.1007/s10765-006-0095-5>

<https://www.doi.org/10.1016/j.ijct.2011.12.009>

<https://www.doi.org/10.1021/ie700759h>

<https://www.doi.org/10.1016/j.ijct.2013.10.026>

<https://www.doi.org/10.1021/ie100508y>

<https://www.doi.org/10.1021/ie700564c>

<https://www.doi.org/10.1016/j.fluid.2018.01.022>

<https://www.doi.org/10.1021/ie800211y>

<https://www.doi.org/10.1016/j.ijct.2011.04.018>

<https://www.choric.org/research/kdb/bcnpn/chownpn.php?cmid=651>

<https://www.doi.org/10.1031/jc700174b>

<https://www.doi.org/10.1031/je501008b>

<https://www.doi.org/10.1016/j.fluid.2019.03.033>

<https://www.doi.org/10.1016/j.ijct.2008.01.004>

<https://www.doi.org/10.1031/jc0405785>

<https://www.doi.org/10.1016/j.fluid.2014.03.006>

<https://www.doi.org/10.1016/j.ijat.2015.05.014>

<https://www.doi.org/10.1031/jc8000021c>

<https://www.doi.org/10.1021/jc800754j>

<https://www.doi.org/10.1016/j.jst.2013.01.010>

<https://www.doi.org/10.1016/j.tsc.2021.10.022>

<https://www.doi.org/10.1016/j.jst.2019.01.003>

<https://www.doi.org/10.1016/j.fluid.2019.104302>

[DOI: 10.1016/j.jmb.2017.09.007](#)

[illegible][illegible]

11. "1910-1911" (1910-1911) 1910-1911

[illegible]

<http://www.dowry.gov.in/2013/07/march-2013-rose/>

<http://www.dcs.gla.ac.uk/~gordon/teaching/2013/2013-04-04/>

[illegible]

<https://www.doi.org/10.1016/j.fluid.2007.08.010>

<https://www.doi.org/10.1021/acs.iced.7b00699>

<https://www.doi.org/10.1016/j.ijct.2015.02.024>

<https://www.doi.org/10.1021/ie0499519>

<https://www.doi.org/10.1021/je5010565>

<https://www.doi.org/10.1016/j.jct.2005.01.015>

<https://www.doi.org/10.1021/je700266n>

<https://www.doi.org/10.1021/je800658v>

<https://www.doi.org/10.1021/je700578f>

<https://www.doi.org/10.1021/ie900048r>

<https://www.doi.org/10.1016/j.ijct.2016.07.017>

<https://www.doi.org/10.1016/j.ijct.2013.02.004>

<https://www.doi.org/10.1016/j.ijct.2015.02.023>

<https://www.doi.org/10.1016/j.ijct.2010.12.004>

<https://www.doi.org/10.1016/j.ijct.2014.04.020>

<https://www.doi.org/10.1021/acs.iced.8b00600>

<https://www.doi.org/10.1021/je0500375>

<https://www.doi.org/10.1021/je049681u>

<https://www.doi.org/10.1021/je800043a>

<https://www.doi.org/10.1016/j.ijct.2005.12.005>

<https://www.doi.org/10.1016/j.ijct.2014.01.023>

<https://www.doi.org/10.1016/j.fluid.2017.06.001>

<https://www.doi.org/10.1016/j.ijct.2016.06.038>

<https://www.doi.org/10.1016/j.fluid.2011.03.033>

<https://www.doi.org/10.1021/ie800376f>

<https://www.doi.org/10.1016/j.fluid.2010.01.036>

<https://www.doi.org/10.1016/j.ijet.2013.05.011>

<https://www.doi.org/10.1021/jc000686n>

<https://www.doi.org/10.1016/j.fluid.2018.01.010>

<https://www.doi.org/10.1016/j.fluid.2013.10.033>

<https://www.doi.org/10.1016/j.fluid.2014.11.030>

<https://www.doi.org/10.1021/jc100002f>

<https://www.doi.org/10.1021/ie101008y>

<https://www.doi.org/10.1016/j.jst.2021.01.011>

<https://www.doi.org/10.4236/ojs.ijed.752054>

<https://www.doi.org/10.1016/j.fluid.2015.06.010>

[illegible][illegible]

111 112 113 114 115 116 117 118 119 120 121 122 123 124 125 126 127 128 129 130 131 132 133 134 135 136 137 138 139 140 141 142 143 144 145 146 147 148 149 150 151 152 153 154 155 156 157 158 159 160 161 162 163 164 165 166 167 168 169 170 171 172 173 174 175 176 177 178 179 180 181 182 183 184 185 186 187 188 189 190 191 192 193 194 195 196 197 198 199 200 201 202 203 204 205 206 207 208 209 210 211 212 213 214 215 216 217 218 219 220 221 222 223 224 225 226 227 228 229 230 231 232 233 234 235 236 237 238 239 240 241 242 243 244 245 246 247 248 249 250 251 252 253 254 255 256 257 258 259 260 261 262 263 264 265 266 267 268 269 270 271 272 273 274 275 276 277 278 279 280 281 282 283 284 285 286 287 288 289 290 291 292 293 294 295 296 297 298 299 300 301 302 303 304 305 306 307 308 309 310 311 312 313 314 315 316 317 318 319 320 321 322 323 324 325 326 327 328 329 330 331 332 333 334 335 336 337 338 339 340 341 342 343 344 345 346 347 348 349 350 351 352 353 354 355 356 357 358 359 360 361 362 363 364 365 366 367 368 369 370 371 372 373 374 375 376 377 378 379 380 381 382 383 384 385 386 387 388 389 390 391 392 393 394 395 396 397 398 399 400 401 402 403 404 405 406 407 408 409 410 411 412 413 414 415 416 417 418 419 420 421 422 423 424 425 426 427 428 429 430 431 432 433 434 435 436 437 438 439 440 441 442 443 444 445 446 447 448 449 450 451 452 453 454 455 456 457 458 459 460 461 462 463 464 465 466 467 468 469 470 471 472 473 474 475 476 477 478 479 480 481 482 483 484 485 486 487 488 489 490 491 492 493 494 495 496 497 498 499 500 501 502 503 504 505 506 507 508 509 510 511 512 513 514 515 516 517 518 519 520 521 522 523 524 525 526 527 528 529 530 531 532 533 534 535 536 537 538 539 540 541 542 543 544 545 546 547 548 549 550 551 552 553 554 555 556 557 558 559 560 561 562 563 564 565 566 567 568 569 570 571 572 573 574 575 576 577 578 579 580 581 582 583 584 585 586 587 588 589 590 591 592 593 594 595 596 597 598 599 600 601 602 603 604 605 606 607 608 609 610 611 612 613 614 615 616 617 618 619 620 621 622 623 624 625 626 627 628 629 630 631 632 633 634 635 636 637 638 639 640 641 642 643 644 645 646 647 648 649 650 651 652 653 654 655 656 657 658 659 660 661 662 663 664 665 666 667 668 669 670 671 672 673 674 675 676 677 678 679 680 681 682 683 684 685 686 687 688 689 690 691 692 693 694 695 696 697 698 699 700 701 702 703 704 705 706 707 708 709 710 711 712 713 714 715 716 717 718 719 720 721 722 723 724 725 726 727 728 729 730 731 732 733 734 735 736 737 738 739 740 741 742 743 744 745 746 747 748 749 750 751 752 753 754 755 756 757 758 759 760 761 762 763 764 765 766 767 768 769 770 771 772 773 774 775 776 777 778 779 780 781 782 783 784 785 786 787 788 789 790 791 792 793 794 795 796 797 798 799 800 801 802 803 804 805 806 807 808 809 810 811 812 813 814 815 816 817 818 819 820 821 822 823 824 825 826 827 828 829 830 831 832 833 834 835 836 837 838 839 840 841 842 843 844 845 846 847 848 849 850 851 852 853 854 855 856 857 858 859 860 861 862 863 864 865 866 867 868 869 870 871 872 873 874 875 876 877 878 879 880 881 882 883 884 885 886 887 888 889 890 891 892 893 894 895 896 897 898 899 900 901 902 903 904 905 906 907 908 909 910 911 912 913 914 915 916 917 918 919 920 921 922 923 924 925 926 927 928 929 930 931 932 933 934 935 936 937 938 939 940 941 942 943 944 945 946 947 948 949 950 951 952 953 954 955 956 957 958 959 960 961 962 963 964 965 966 967 968 969 970 971 972 973 974 975 976 977 978 979 980 981 982 983 984 985 986 987 988 989 990 991 992 993 994 995 996 997 998 999 1000 1001 1002 1003 1004 1005 1006 1007 1008 1009 1010 1011 1012 1013 1014 1015 1016 1017 1018 1019 1020 1021 1022 1023 1024 1025 1026 1027 1028 1029 1030 1031 1032 1033 1034 1035 1036 1037 1038 1039 1040 1041 1042 1043 1044 1045 1046 1047 1048 1049 1050 1051 1052 1053 1054 1055 1056 1057 1058 1059 1060 1061 1062 1063 1064 1065 1066 1067 1068 1069 1070 1071 1072 1073 1074 1075 1076 1077 1078 1079 1080 1081 1082 1083 1084 1085 1086 1087 1088 1089 1090 1091 1092 1093 1094 1095 1096 1097 1098 1099 1100 1101 1102 1103 1104 1105 1106 110

<http://www.ncbi.nlm.nih.gov/pmc/articles/PMC3030303/>

<https://www.industry.gov.au/publications/industry-4.0-2024-2025>

<https://www.nasa.gov/press/20160501.nasa-releases-new-3d-model-of-planet-venus/>

<https://www.industry.gov.au/publications/industry-2019-2020>

<https://www.nasa.gov/press/2019/jan12/earth-2019-01-12-01>

Measurement and Correlation of Bubble Point Pressure in (CO₂ + C₆H₆), (CO₂ + CH₃COCH₃), (CO₂ + C₆H₁₂) and (CO₂ + C₈H₁₈) and (CO₂ + C₁₀H₂₂) and (CO₂ + C₁₂H₂₆) and (CO₂ + C₁₄H₃₀) and (CO₂ + C₁₆H₃₄) and (CO₂ + C₁₈H₃₈) and (CO₂ + C₂₀H₄₂) and (CO₂ + C₂₂H₄₆) and (CO₂ + C₂₄H₅₀) and (CO₂ + C₂₆H₅₄) and (CO₂ + C₂₈H₅₈) and (CO₂ + C₃₀H₆₂) and (CO₂ + C₃₂H₆₆) and (CO₂ + C₃₄H₇₀) and (CO₂ + C₃₆H₇₄) and (CO₂ + C₃₈H₇₈) and (CO₂ + C₄₀H₈₂) and (CO₂ + C₄₂H₈₆) and (CO₂ + C₄₄H₉₀) and (CO₂ + C₄₆H₉₄) and (CO₂ + C₄₈H₉₈) and (CO₂ + C₅₀H₁₀₂) and (CO₂ + C₅₂H₁₀₆) and (CO₂ + C₅₄H₁₁₀) and (CO₂ + C₅₆H₁₁₄) and (CO₂ + C₅₈H₁₁₈) and (CO₂ + C₆₀H₁₂₂) and (CO₂ + C₆₂H₁₂₆) and (CO₂ + C₆₄H₁₃₀) and (CO₂ + C₆₆H₁₃₄) and (CO₂ + C₆₈H₁₃₈) and (CO₂ + C₇₀H₁₄₂) and (CO₂ + C₇₂H₁₄₆) and (CO₂ + C₇₄H₁₅₀) and (CO₂ + C₇₆H₁₅₄) and (CO₂ + C₇₈H₁₅₈) and (CO₂ + C₈₀H₁₆₂) and (CO₂ + C₈₂H₁₆₆) and (CO₂ + C₈₄H₁₇₀) and (CO₂ + C₈₆H₁₇₄) and (CO₂ + C₈₈H₁₇₈) and (CO₂ + C₉₀H₁₈₂) and (CO₂ + C₉₂H₁₈₆) and (CO₂ + C₉₄H₁₉₀) and (CO₂ + C₉₆H₁₉₄) and (CO₂ + C₉₈H₁₉₈) and (CO₂ + C₁₀₀H₂₀₂) and (CO₂ + C₁₀₂H₂₀₆) and (CO₂ + C₁₀₄H₂₁₀) and (CO₂ + C₁₀₆H₂₁₄) and (CO₂ + C₁₀₈H₂₁₈) and (CO₂ + C₁₁₀H₂₂₂) and (CO₂ + C₁₁₂H₂₂₆) and (CO₂ + C₁₁₄H₂₃₀) and (CO₂ + C₁₁₆H₂₃₄) and (CO₂ + C₁₁₈H₂₃₈) and (CO₂ + C₁₂₀H₂₄₂) and (CO₂ + C₁₂₂H₂₄₆) and (CO₂ + C₁₂₄H₂₅₀) and (CO₂ + C₁₂₆H₂₅₄) and (CO₂ + C₁₂₈H₂₅₈) and (CO₂ + C₁₃₀H₂₆₂) and (CO₂ + C₁₃₂H₂₆₆) and (CO₂ + C₁₃₄H₂₇₀) and (CO₂ + C₁₃₆H₂₇₄) and (CO₂ + C₁₃₈H₂₇₈) and (CO₂ + C₁₄₀H₂₈₂) and (CO₂ + C₁₄₂H₂₈₆) and (CO₂ + C₁₄₄H₂₉₀) and (CO₂ + C₁₄₆H₂₉₄) and (CO₂ + C₁₄₈H₂₉₈) and (CO₂ + C₁₅₀H₃₀₂) and (CO₂ + C₁₅₂H₃₀₆) and (CO₂ + C₁₅₄H₃₁₀) and (CO₂ + C₁₅₆H₃₁₄) and (CO₂ + C₁₅₈H₃₁₈) and (CO₂ + C₁₆₀H₃₂₂) and (CO₂ + C₁₆₂H₃₂₆) and (CO₂ + C₁₆₄H₃₃₀) and (CO₂ + C₁₆₆H₃₃₄) and (CO₂ + C₁₆₈H₃₃₈) and (CO₂ + C₁₇₀H₃₄₂) and (CO₂ + C₁₇₂H₃₄₆) and (CO₂ + C₁₇₄H₃₅₀) and (CO₂ + C₁₇₆H₃₅₄) and (CO₂ + C₁₇₈H₃₅₈) and (CO₂ + C₁₈₀H₃₆₂) and (CO₂ + C₁₈₂H₃₆₆) and (CO₂ + C₁₈₄H₃₇₀) and (CO₂ + C₁₈₆H₃₇₄) and (CO₂ + C₁₈₈H₃₇₈) and (CO₂ + C₁₉₀H₃₈₂) and (CO₂ + C₁₉₂H₃₈₆) and (CO₂ + C₁₉₄H₃₉₀) and (CO₂ + C₁₉₆H₃₉₄) and (CO₂ + C₁₉₈H₃₉₈) and (CO₂ + C₂₀₀H₄₀₂) and (CO₂ + C₂₀₂H₄₀₆) and (CO₂ + C₂₀₄H₄₁₀) and (CO₂ + C₂₀₆H₄₁₄) and (CO₂ + C₂₀₈H₄₁₈) and (CO₂ + C₂₁₀H₄₂₂) and (CO₂ + C₂₁₂H₄₂₆) and (CO₂ + C₂₁₄H₄₃₀) and (CO₂ + C₂₁₆H₄₃₄) and (CO₂ + C₂₁₈H₄₃₈) and (CO₂ + C₂₂₀H₄₄₂) and (CO₂ + C₂₂₂H₄₄₆) and (CO₂ + C₂₂₄H₄₅₀) and (CO₂ + C₂₂₆H₄₅₄) and (CO₂ + C₂₂₈H₄₅₈) and (CO₂ + C₂₃₀H₄₆₂) and (CO₂ + C₂₃₂H₄₆₆) and (CO₂ + C₂₃₄H₄₇₀) and (CO₂ + C₂₃₆H₄₇₄) and (CO₂ + C₂₃₈H₄₇₈) and (CO₂ + C₂₄₀H₄₈₂) and (CO₂ + C₂₄₂H₄₈₆) and (CO₂ + C₂₄₄H₄₉₀) and (CO₂ + C₂₄₆H₄₉₄) and (CO₂ + C₂₄₈H₄₉₈) and (CO₂ + C₂₅₀H₅₀₂) and (CO₂ + C₂₅₂H₅₀₆) and (CO₂ + C₂₅₄H₅₁₀) and (CO₂ + C₂₅₆H₅₁₄) and (CO₂ + C₂₅₈H₅₁₈) and (CO₂ + C₂₆₀H₅₂₂) and (CO₂ + C₂₆₂H₅₂₆) and (CO₂ + C₂₆₄H₅₃₀) and (CO₂ + C₂₆₆H₅₃₄) and (CO₂ + C₂₆₈H₅₃₈) and (CO₂ + C₂₇₀H₅₄₂) and (CO₂ + C₂₇₂H₅₄₆) and (CO₂ + C₂₇₄H₅₅₀) and (CO₂ + C₂₇₆H₅₅₄) and (CO₂ + C₂₇₈H

<https://www.doi.org/10.1021/je900312z>

<https://www.doi.org/10.1016/j.fluid.2008.09.005>

<https://www.doi.org/10.1021/acs.jced.5b00009>

<https://www.doi.org/10.1021/ie060289l>

<https://www.doi.org/10.1016/j.ijct.2009.10.010>

<https://www.doi.org/10.1016/j.ijct.2015.08.017>

<https://www.doi.org/10.1007/s10765-007-0223-x>

<https://www.doi.org/10.1021/acs.jced.7b00244>

<https://www.doi.org/10.1021/ie800157v>

<https://www.doi.org/10.1016/j.ijct.2013.10.017>

<https://www.doi.org/10.1016/j.tca.2013.01.028>

<https://www.doi.org/10.1016/j.ijct.2009.07.010>

<https://www.doi.org/10.1016/j.fluid.2018.11.025>

<https://www.doi.org/10.1016/j.ijct.2013.01.007>

<https://www.doi.org/10.1021/je060026r>

<https://www.doi.org/10.1016/j.fluid.2008.09.018>

<https://www.doi.org/10.1021/ie2009736>

<https://www.doi.org/10.1021/ie900838a>

<https://www.doi.org/10.1016/j.fluid.2011.05.003>

<https://www.doi.org/10.1016/j.fluid.2009.05.006>

<https://www.doi.org/10.1016/j.fluid.2008.10.008>

<https://www.doi.org/10.1016/j.fluid.2005.07.013>

<https://www.doi.org/10.1016/j.fluid.2013.05.003>

<https://www.doi.org/10.1031/jc4010917>

phosphoramidic

<https://www.doi.org/10.1021/jc400502a>

<https://www.doi.org/10.1016/j.tsc.2025.10.008>

<https://www.doi.org/10.1031/acs.joc.4b00837>

<https://www.doi.org/10.1001/jco.100716>

<https://www.doi.org/10.1016/j.fluid.2018.03.021>

DOI: 10.1016/j.jmb.2017.08.009

<https://doi.org/10.1016/j.jmb.2022.107900>

<https://doi.org/10.1001/ja.5000001>

1997-1998, 1999-2000, 2001-2002, 2003-2004, 2005-2006, 2007-2008, 2009-2010, 2011-2012, 2013-2014, 2015-2016, 2017-2018, 2019-2020, 2021-2022, 2023-2024, 2025-2026, 2027-2028, 2029-2030, 2031-2032, 2033-2034, 2035-2036, 2037-2038, 2039-2040, 2041-2042, 2043-2044, 2045-2046, 2047-2048, 2049-2050, 2051-2052, 2053-2054, 2055-2056, 2057-2058, 2059-2060, 2061-2062, 2063-2064, 2065-2066, 2067-2068, 2069-2070, 2071-2072, 2073-2074, 2075-2076, 2077-2078, 2079-2080, 2081-2082, 2083-2084, 2085-2086, 2087-2088, 2089-2090, 2091-2092, 2093-2094, 2095-2096, 2097-2098, 2099-2100, 2101-2102, 2103-2104, 2105-2106, 2107-2108, 2109-2110, 2111-2112, 2113-2114, 2115-2116, 2117-2118, 2119-2120, 2121-2122, 2123-2124, 2125-2126, 2127-2128, 2129-2130, 2131-2132, 2133-2134, 2135-2136, 2137-2138, 2139-2140, 2141-2142, 2143-2144, 2145-2146, 2147-2148, 2149-2150, 2151-2152, 2153-2154, 2155-2156, 2157-2158, 2159-2160, 2161-2162, 2163-2164, 2165-2166, 2167-2168, 2169-2170, 2171-2172, 2173-2174, 2175-2176, 2177-2178, 2179-2180, 2181-2182, 2183-2184, 2185-2186, 2187-2188, 2189-2190, 2191-2192, 2193-2194, 2195-2196, 2197-2198, 2199-2200, 2201-2202, 2203-2204, 2205-2206, 2207-2208, 2209-2210, 2211-2212, 2213-2214, 2215-2216, 2217-2218, 2219-2220, 2221-2222, 2223-2224, 2225-2226, 2227-2228, 2229-2230, 2231-2232, 2233-2234, 2235-2236, 2237-2238, 2239-2240, 2241-2242, 2243-2244, 2245-2246, 2247-2248, 2249-2250, 2251-2252, 2253-2254, 2255-2256, 2257-2258, 2259-2260, 2261-2262, 2263-2264, 2265-2266, 2267-2268, 2269-2270, 2271-2272, 2273-2274, 2275-2276, 2277-2278, 2279-2280, 2281-2282, 2283-2284, 2285-2286, 2287-2288, 2289-2290, 2291-2292, 2293-2294, 2295-2296, 2297-2298, 2299-2300, 2301-2302, 2303-2304, 2305-2306, 2307-2308, 2309-2310, 2311-2312, 2313-2314, 2315-2316, 2317-2318, 2319-2320, 2321-2322, 2323-2324, 2325-2326, 2327-2328, 2329-2330, 2331-2332, 2333-2334, 2335-2336, 2337-2338, 2339-2340, 2341-2342, 2343-2344, 2345-2346, 2347-2348, 2349-2350, 2351-2352, 2353-2354, 2355-2356, 2357-2358, 2359-2360, 2361-2362, 2363-2364, 2365-2366, 2367-2368, 2369-2370, 2371-2372, 2373-2374, 2375-2376, 2377-2378, 2379-2380, 2381-2382, 2383-2384, 2385-2386, 2387-2388, 2389-2390, 2391-2392, 2393-2394, 2395-2396, 2397-2398, 2399-2400, 2401-2402, 2403-2404, 2405-2406, 2407-2408, 2409-2410, 2411-2412, 2413-2414, 2415-2416, 2417-2418, 2419-2420, 2421-2422, 2423-2424, 2425-2426, 2427-2428, 2429-2430, 2431-2432, 2433-2434, 2435-2436, 2437-2438, 2439-2440, 2441-2442, 2443-2444, 2445-2446, 2447-2448, 2449-2450, 2451-2452, 2453-2454, 2455-2456, 2457-2458, 2459-2460, 2461-2462, 2463-2464, 2465-2466, 2467-2468, 2469-2470, 2471-2472, 2473-2474, 2475-2476, 2477-2478, 2479-2480, 2481-2482, 2483-2484, 2485-2486, 2487-2488, 2489-2490, 2491-2492, 2493-2494, 2495-2496, 2497-2498, 2499-2500, 2501-2502, 2503-2504, 2505-2506, 2507-2508, 2509-2510, 2511-2512, 2513-2514, 2515-2516, 2517-2518, 2519-2520, 2521-2522, 2523-2524, 2525-2526, 2527-2528, 2529-2530, 2531-2532, 2533-2534, 2535-2536, 2537-2538, 2539-2540, 2541-2542, 2543-2544, 2545-2546, 2547-2548, 2549-2550, 2551-2552, 2553-2554, 2555-2556, 2557-2558, 2559-2560, 2561-2562, 2563-2564, 2565-2566, 2567-2568, 2569-2570, 2571-2572, 2573-2574, 2575-2576, 2577-2578, 2579-2580, 2581-2582, 2583-2584, 2585-2586, 2587-2588, 2589-2590, 2591-2592, 2593-2594, 2595-2596, 2597-2598, 2599-2600, 2601-2602, 2603-2604, 2605-2606, 2607-2608, 2609-2610, 2611-2612, 2613-2614, 2615-2616, 2617-2618, 2619-2620, 2621-2622, 2623-2624, 2625-2626, 2627-2628, 2629-2630, 2631-2632, 2633-2634, 2635-2636, 2637-2638, 2639-2640, 2641-2642, 2643-2644, 2645-2646, 2647-2648, 2649-2650, 2651-2652, 2653-2654, 2655-2656, 2657-2658, 2659-2660, 2661-2662, 2663-2664, 2665-2666, 2667-2668, 2669-2670, 2671-2672, 2673-2674, 2675-2676, 2677-2678, 2679-2680, 2681-2682, 2683-2684, 2685-2686, 2687-2688, 2689-2690, 2691-2692, 2693-2694, 2695-2696, 2697-2698, 2699-2700, 2701-2702, 2703-2704, 2705-2706, 2707-2708, 2709-2710, 2711-2712, 2713-2714, 2715-2716, 2717-2718, 2719-2720, 2721-2722, 2723-2724, 2725-2726, 2727-2728, 2729-2730, 2731-2732, 2733-2734, 2735-2736, 2737-2738, 2739-2740, 27

14. // 1.1. 1991/5 000005

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doi:10.1371/journal.pone.0131472.g002

doi:10.1371/journal.pone.0142123.g002

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<https://www.ackery.org/for-cc0/516133-5171-5551-5>

http://www.wadsworth.com/ENR_LLEP/VOL2/VOL2_026

<https://www.doi.org/10.1016/j.jclepro.2019.119033>

<https://www.wadenerg.com/energy/journals/2020/03/01>

[illegible]

<https://www.doi.org/10.1016/j.ijct.2018.07.024>

<https://www.doi.org/10.1021/ie5009558>

<https://www.doi.org/10.1007/s10765-006-0063-0>

<https://www.doi.org/10.1016/j.fluid.2005.06.011>

<https://www.doi.org/10.1016/j.jct.2010.01.006>

http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl_file/ci034243xsi20040112_053635.txt

<https://www.doi.org/10.1021/acs.jced.8b00632>

<https://www.doi.org/10.1021/ie025609p>

<https://www.doi.org/10.1021/ie400061z>

<https://www.doi.org/10.1016/j.fluid.2004.07.013>

<https://www.doi.org/10.1016/j.ijct.2017.11.017>

<https://www.doi.org/10.1016/j.tca.2005.08.012>

<https://www.doi.org/10.1021/je1011604>

<https://www.doi.org/10.1016/j.fluid.2006.07.015>

<https://www.doi.org/10.1021/ie050146i>

<https://www.doi.org/10.1016/j.ijct.2005.03.006>

<https://www.doi.org/10.1016/j.fluid.2014.07.034>

<https://www.doi.org/10.1016/j.ijct.2016.02.027>

<https://www.doi.org/10.1021/ie034189a>

<https://www.doi.org/10.1016/j.ijct.2018.09.023>

<https://www.doi.org/10.1021/acs.iced.8b00080>

<https://www.doi.org/10.1016/j.ijct.2009.03.009>

<https://www.doi.org/10.1016/j.fluid.2006.03.003>

<https://www.doi.org/10.1031/acs.iced.5b00770>

<https://www.doi.org/10.1016/j.fluid.2014.01.033>

<https://www.doi.org/10.1016/j.fluid.2014.13.003>

<https://www.doi.org/10.1031/jc060441i>

<https://www.doi.org/10.1031/jc300050a>

<https://www.doi.org/10.1016/j.fluid.2011.01.007>

<https://www.doi.org/10.1021/jc700130n>

<https://www.doi.org/10.1021/jc000600f>

amide
<https://www.doi.org/10.1016/j.fluid.2003.03.002>

<https://www.doi.org/10.1016/j.jst.2020.12.004>

<https://www.doi.org/10.1016/j.fluid.2015.01.005>

<https://www.doi.org/10.1016/j.fluid.2022.103102>

<https://www.doi.org/10.1016/j.jst.2016.03.002>

11. // 11.1010" 11.1017 10.000

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11. "11-10-10" 511-0007-01-010

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Downloaded from <http://ajph.org/> on November 10, 2015

[illegible]

[illegible]

<https://www.doi.org/10.1021/acs.jced.8b00659>

<https://www.doi.org/10.1021/acs.iced.8b00635>

<https://www.doi.org/10.1016/j.jct.2006.06.002>

<https://www.doi.org/10.1021/je034005y>

<https://www.doi.org/10.1021/je900807v>

<https://www.doi.org/10.1016/j.fluid.2007.03.013>

<https://www.doi.org/10.1016/j.jct.2015.06.023>

<https://www.doi.org/10.1016/j.jct.2011.11.021>

<https://www.doi.org/10.1016/j.fluid.2006.04.016>

<https://www.doi.org/10.1021/acs.jced.9b00064>

<https://www.doi.org/10.1016/j.tca.2015.04.011>

<https://www.doi.org/10.1016/j.jct.2004.07.024>

<https://www.doi.org/10.1016/j.fluid.2005.11.014>

<https://www.doi.org/10.1016/j.ijct.2016.09.021>

<https://www.doi.org/10.1021/ie8006309>

<https://www.doi.org/10.1016/j.ijct.2011.11.025>

<http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDataset002.xlsx>

<https://www.doi.org/10.1016/j.ijct.2016.01.017>

<https://www.doi.org/10.1021/je700426k>

<https://www.doi.org/10.1016/j.fluid.2016.02.028>

<https://www.doi.org/10.1016/j.fluid.2012.04.008>

<https://www.doi.org/10.1016/j.ijct.2005.03.007>

<https://www.doi.org/10.1016/j.tsc.2006.06.018>

<https://www.doi.org/10.1021/ie060350m>

<https://www.doi.org/10.1016/j.fluid.2018.11.011>

<https://www.doi.org/10.1021/ie034022p>

<https://www.doi.org/10.1016/j.fluid.2010.08.016>

<https://www.doi.org/10.1016/j.ijct.2014.12.014>

<https://www.doi.org/10.1016/j.ijct.2015.12.037>

<https://www.doi.org/10.1031/jc800049b>

<https://www.doi.org/10.1031/jc501065a>

<https://www.doi.org/10.1016/j.fluid.2009.09.034>

<https://www.doi.org/10.1016/j.itcc.2013.04.003>

<https://www.doi.org/10.1021/jc800023c>

<https://www.doi.org/10.1031/jc050544m>

<https://www.doi.org/10.1016/j.iast.2014.06.006>

<https://www.doi.org/10.1016/j.jst.2020.06.011>

<https://www.doi.org/10.1001/ja.0242041>

<https://doi.org/10.1001/ja.20000001>

<https://www.doi.org/10.1001/ja.20003141>

<https://www.doi.org/10.1016/j.jst.2020.05.002>

<https://www.doi.org/10.1016/j.fluc.2022.11.005>

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<https://www.doi.org/10.1016/j.fluid.2015.12.009>

<https://www.doi.org/10.1016/j.fluid.2009.06.015>

<https://www.doi.org/10.1016/j.ijct.2007.10.010>

<https://www.doi.org/10.1016/j.ijct.2005.07.004>

<https://www.doi.org/10.1021/je800218a>

<https://www.doi.org/10.1016/j.fluid.2010.01.025>

<https://www.doi.org/10.1021/acs.iced.9b00059>

<https://www.doi.org/10.1021/je6005604>

<https://www.doi.org/10.1016/j.fluid.2013.09.048>

<https://www.doi.org/10.1016/j.fluid.2016.02.006>

<https://www.doi.org/10.1016/j.ijct.2016.07.021>

<https://www.doi.org/10.1021/ie900277m>

<https://www.doi.org/10.1021/je700209v>

<https://www.doi.org/10.1021/je100952p>

<https://www.doi.org/10.1016/j.ijct.2007.09.002>

<https://www.doi.org/10.1016/j.fluid.2018.09.024>

<https://www.doi.org/10.1021/ie050394f>

<https://www.doi.org/10.1016/j.ijct.2015.01.003>

<https://www.doi.org/10.1021/je1009812>

<https://www.doi.org/10.1007/s10765-009-0562-x>

<https://www.doi.org/10.1021/ie800846i>

<https://www.doi.org/10.1016/j.ijct.2010.06.009>

<https://www.doi.org/10.1016/j.ijct.2008.08.004>

<https://www.doi.org/10.1021/jo8009132>

<https://www.doi.org/10.1016/j.ijct.2017.13.013>

<http://link.springer.com/article/10.1007/BF02311732>

<https://www.doi.org/10.1016/j.ijet.2003.11.003>

<https://www.doi.org/10.1016/j.fluid.2008.01.007>

<https://www.doi.org/10.1007/s10365-013-1526-8>

<https://www.doi.org/10.1016/j.ijet.2009.08.013>

<https://www.doi.org/10.1021/jc060220f>

<https://www.elsevier.com/locate/jlth/harper/shawwpr-prb2amid-651>

<https://www.doi.org/10.1021/acs.024025a>

<https://www.doi.org/10.1001/ja.300070>

<https://www.doi.org/10.1001/ja.010217>

<https://www.doi.org/10.1016/j.jst.2024.03.001>

L'Espresso

[illegible][illegible]

<http://www.rockwell.com/1919-1921/0500554>

<https://www.industry.gov.au/publications/industry-100-top-100-companies-in-australia-2019>

<https://www.doh.gov/press/press-releases/2020/04/04/2020-04-04-01>

<https://www.doi.org/10.1016/j.jmoldi.2008.11.001>

[illegible]

<https://www.doi.org/10.1021/je900237e>

<https://www.doi.org/10.1021/je100341q>

<https://www.doi.org/10.1016/j.jct.2006.05.006>

<https://www.doi.org/10.1016/j.jct.2007.11.009>

<https://www.doi.org/10.1016/j.fluid.2009.08.017>

<https://www.doi.org/10.1016/j.fluid.2015.09.030>

<https://www.doi.org/10.1016/j.fluid.2009.03.012>

<https://www.doi.org/10.1021/ie100998r>

<https://www.doi.org/10.1016/j.ijct.2010.05.017>

<https://www.doi.org/10.1016/j.fluid.2013.11.034>

<https://www.doi.org/10.1021/ie200266f>

<https://www.doi.org/10.1016/j.fluid.2019.03.022>

<https://www.doi.org/10.1021/ie050231r>

<https://www.doi.org/10.1016/j.ijct.2014.05.020>

<https://www.doi.org/10.1016/j.ijct.2011.12.006>

<https://www.doi.org/10.1021/je100489z>

<https://www.doi.org/10.1016/j.ijct.2012.02.032>

<https://www.doi.org/10.1021/je7001682>

<https://www.doi.org/10.1007/s10765-009-0625-z>

<https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure>

<https://www.doi.org/10.1016/j.ijct.2010.01.004>

<https://www.doi.org/10.1021/je2013582>

<https://www.doi.org/10.1016/j.fluid.2010.08.031>

<https://www.doi.org/10.1031/jc500443m>

<https://www.doi.org/10.1016/j.ijct.2011.08.038>

<https://www.doi.org/10.1016/j.ijct.2015.11.016>

<https://www.doi.org/10.1016/j.ijet.2005.03.003>

<https://www.doi.org/10.1021/jc401098b>

<https://www.doi.org/10.1021/jc300414c>

<https://www.doi.org/10.1021/jc060475r>

<https://www.doi.org/10.1021/jc0002724>

<https://www.doi.org/10.1031/acs.joc.5b00380>

<https://www.doi.org/10.1021/acs.050140b>

<https://www.doi.org/10.1016/j.fluid.2019.07.022>

<https://www.doi.org/10.1016/j.jst.2022.20.014>

<https://www.doi.org/10.1001/psap.2021.00011>

11. // 11.10.10 // 10.10.10 // 0010 00 0101

11. // 11.10.1991/ 11.10.1991

"I'm not going to let you go," said the man.

<https://www.industry.gov.au/publications/10-1010/11-0001>

<https://www.industry.gov.au/publications/2019-05-09>

<https://www.industry.gov.au/publications/2019-03-20-01>

<https://www.ncbi.nlm.nih.gov/pmc/articles/PMC6055130/>

<https://www.doi.org/10.1016/j.jmval.2019.100103>

Legend

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
cps:	Solid phase heat capacity
dm:	Dipole Moment

<https://www.doi.org/10.1021/je700539w>
<https://www.doi.org/10.1021/je0502896>
<https://www.doi.org/10.1016/j.jct.2018.09.003>
<https://www.doi.org/10.1021/je200628n>
<https://www.doi.org/10.1021/je0602972>
<https://www.doi.org/10.1016/j.fluid.2014.06.021>
<https://www.doi.org/10.1016/j.jct.2010.12.005>
<https://www.doi.org/10.1007/s10765-008-0390-4>
<https://www.doi.org/10.1016/j.jct.2012.01.004>
<https://www.doi.org/10.1016/j.jct.2013.09.007>
<https://www.doi.org/10.1021/je900641w>
<https://www.doi.org/10.1021/je049875+>
<https://www.doi.org/10.1021/je200822w>
<https://www.doi.org/10.1016/j.jct.2012.05.017>
<https://www.doi.org/10.1021/je0341920>
<https://www.doi.org/10.1021/acs.jced.7b00119>
<https://www.doi.org/10.1021/je0602723>
<https://www.doi.org/10.1016/j.fluid.2006.01.014>
<https://www.doi.org/10.1021/je900321j>
<https://www.doi.org/10.1021/je0602263>
<http://webbook.nist.gov/cgi/cbook.cgi?ID=C71432&Units=SI>
<https://www.doi.org/10.1021/je700034q>
<https://www.doi.org/10.1021/je020196d>
<https://www.doi.org/10.1021/je100517z>
<https://www.doi.org/10.1021/je060153n>
<https://www.doi.org/10.1021/je0502546>
<https://www.doi.org/10.1021/acs.jced.6b00655>
<https://www.doi.org/10.1021/je200195q>
<https://www.doi.org/10.1016/j.jct.2018.08.028>
<https://www.doi.org/10.1016/j.tca.2012.08.011>

dvisc:	Dynamic viscosity
fl:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hsub:	Enthalpy of sublimation at standard conditions
hsubt:	Enthalpy of sublimation at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
psub:	Sublimation pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhof:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
ss:	Solid phase molar entropy at standard conditions
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tfp:	Melting point
vc:	Critical Volume
vols:	Specific Volume

zc: Critical Compressibility
zra: Rackett Parameter

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